

NOMENCLATURE

B	= Formation Volume Factor	(Res Vol/Std Vol)
c_t	= System Total Compressibility	(Vol/Vol)/psi
DR	= Damage Ratio	
h	= Estimated Net Pay Thickness	Ft
k	= Permeability	md
m	{	
	= (Liquid) Slope Extrapolated Pressure Plot	psi/cycle
	= (Gas) Slope Extrapolated m(P) Plot	MM psi ² /cp/cycle
m(P*)	= Real Gas Potential at P*	MM psi ² /cp
m(P _f)	= Real Gas Potential at P _f	MM psi ² /cp
AOF ₁	= Maximum Indicated Absolute Open Flow at Test Conditions	MCFD
AOF ₂	= Minimum Indicated Absolute Open Flow at Test Conditions	MCFD
P*	= Extrapolated Static Pressure	Psig
P _f	= Final Flow Pressure	Psig
Q	= Liquid Production Rate During Test	BPD
Q ₁	= Theoretical Liquid Production w/Damage Removed	BPD
Q _g	= Measured Gas Production Rate	MCFD
r _i	= Approximate Radius of Investigation	Ft
r _w	= Radius of Well Bore	Ft
S	= Skin Factor	
t	= Total Flow Time Previous to Closed-in	Minutes
Δt	= Closed-in Time at Data Point	Minutes
T	= Temperature Rankine	°R
φ	= Porosity (fraction)	
μ	= Viscosity of Gas or Liquid	cp
Log	= Common Log	



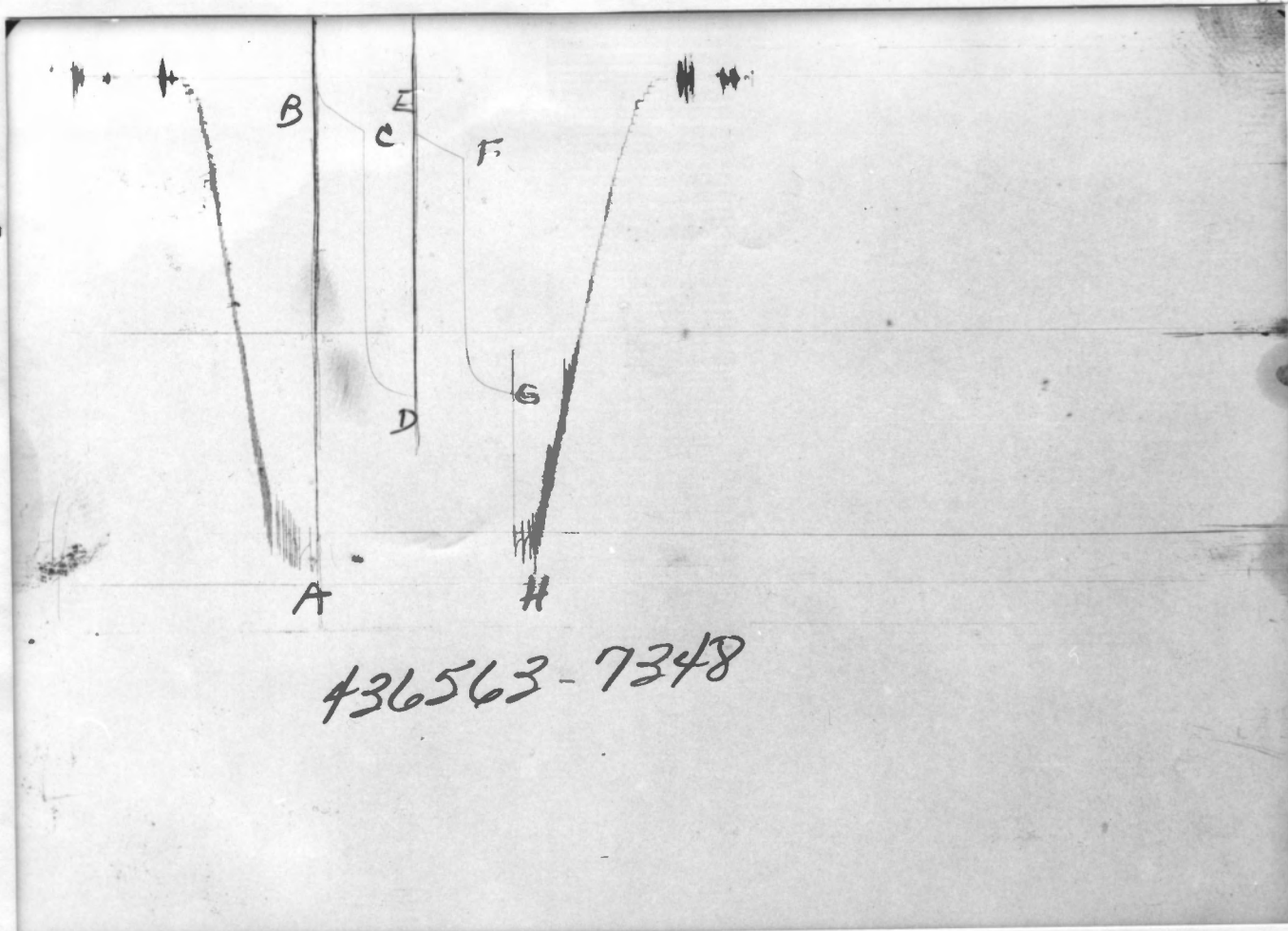
TICKET NO. 43656300

12-SEP-86

PRATT

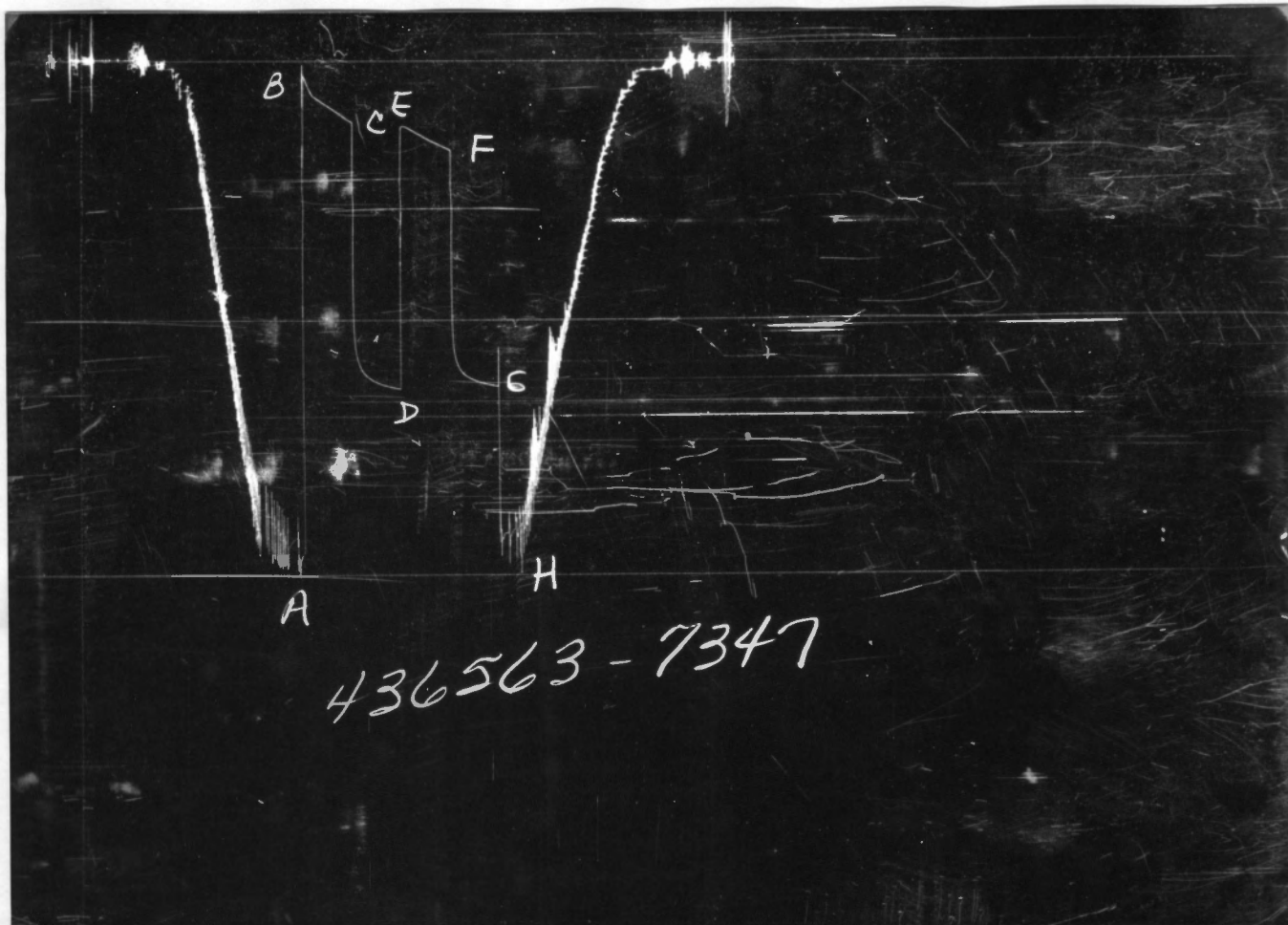
FORMATION TESTING SERVICE REPORT

LEASE NAME	WELL NO.	TEST NO.	TESTED INTERVAL	MC NEISH OIL OPERATIONS
LEASE NO. - 3-255-15V	1	1	3874.0 - 3925.0	LEASE OWNER/COMPANY NAME
LEGAL LOCATION	FIELD	COUNTY	STATE	IC
SEC. - 15V - RING	PRATT	STAFFORD	KANSAS	



GAUGE NO: 7348 DEPTH: 3853.0 BLANKED OFF: NO HOUR OF CLOCK: 12

ID	DESCRIPTION	PRESSURE		TIME		TYPE
		REPORTED	CALCULATED	REPORTED	CALCULATED	
A	INITIAL HYDROSTATIC		1838.0			
B	INITIAL FIRST FLOW		20.1			
C	FINAL FIRST FLOW		207.5	30.0	30.1	F
C	INITIAL FIRST CLOSED-IN		207.5			
D	FINAL FIRST CLOSED-IN		1250.1	30.0	29.0	C
E	INITIAL SECOND FLOW		221.8			
F	FINAL SECOND FLOW		312.4	30.0	30.9	F
F	INITIAL SECOND CLOSED-IN		312.4			
G	FINAL SECOND CLOSED-IN		1239.5	30.0	28.6	C
H	FINAL HYDROSTATIC		1819.9			



GAUGE NO: 7347 DEPTH: 3922.0 BLANKED OFF: YES HOUR OF CLOCK: 12

ID	DESCRIPTION	PRESSURE		TIME		TYPE
		REPORTED	CALCULATED	REPORTED	CALCULATED	
A	INITIAL HYDROSTATIC	1863	1856.1			
B	INITIAL FIRST FLOW	39	56.4	30.0	30.1	F
C	FINAL FIRST FLOW	232	236.2			
C	INITIAL FIRST CLOSED-IN	232	236.2	30.0	29.0	C
D	FINAL FIRST CLOSED-IN	1287	1276.2			
E	INITIAL SECOND FLOW	232	255.2	30.0	30.9	F
F	FINAL SECOND FLOW	329	340.4			
F	INITIAL SECOND CLOSED-IN	329	340.4	30.0	28.6	C
G	FINAL SECOND CLOSED-IN	1249	1266.8			
H	FINAL HYDROSTATIC	1863	1840.1			

EQUIPMENT & HOLE DATA

FORMATION TESTED: KANSAS CITY
NET PAY (ft): _____
GROSS TESTED FOOTAGE: 51.0
ALL DEPTHS MEASURED FROM: KELLY BUSHING
CASING PERFS. (ft): _____
HOLE OR CASING SIZE (in): 7.875
ELEVATION (ft): 2040.0
TOTAL DEPTH (ft): 3925.0
PACKER DEPTH(S) (ft): 3868, 3874
FINAL SURFACE CHOKE (in): _____
BOTTOM HOLE CHOKE (in): 0.750
MUD WEIGHT (lb/gal): _____
MUD VISCOSITY (sec): _____
ESTIMATED HOLE TEMP. (°F): _____
ACTUAL HOLE TEMP. (°F): 115 @ 3920.0 ft

TICKET NUMBER: 43656300

DATE: 9-8-86 TEST NO: 1

TYPE DST: OPEN HOLE

HALLIBURTON CAMP:
PRATT

TESTER: L. R. PARKER

WITNESS: M. DUBOIS

DRILLING CONTRACTOR:
EAGLE DRILLING COMPANY

FLUID PROPERTIES FOR RECOVERED MUD & WATER

SOURCE	RESISTIVITY	CHLORIDES
<u>PIT</u>	<u> </u> @ <u> </u> °F	<u>140000</u> ppm
<u>TOP</u>	<u> </u> @ <u> </u> °F	<u>29000</u> ppm
<u>MIDDLE</u>	<u> </u> @ <u> </u> °F	<u>36000</u> ppm
<u>BOTTOM</u>	<u> </u> @ <u> </u> °F	<u>97650</u> ppm
_____	<u> </u> @ <u> </u> °F	<u> </u> ppm
_____	<u> </u> @ <u> </u> °F	<u> </u> ppm

SAMPLER DATA

Psig AT SURFACE: _____
cu.ft. OF GAS: _____
cc OF OIL: _____
cc OF WATER: _____
cc OF MUD: _____
TOTAL LIQUID cc: _____

HYDROCARBON PROPERTIES

OIL GRAVITY (°API): _____ @ _____ °F
GAS/OIL RATIO (cu.ft. per bbl): _____
GAS GRAVITY: _____

CUSHION DATA

TYPE	AMOUNT	WEIGHT
_____	_____	_____
_____	_____	_____

RECOVERED:

90 FEET OF MUDDY WATER
540 FEET OF WATER

MEASURED FROM
TESTER VALVE

REMARKS:

TICKET NO: 43656300

CLOCK NO: 26864 HOUR: 12



GAUGE NO: 7348

DEPTH: 3853.0

REF	MINUTES	PRESSURE	ΔP	$\frac{t \times \Delta t}{t + \Delta t}$	$\log \frac{t + \Delta t}{\Delta t}$
FIRST FLOW					
B 1	0.0	20.1			
2	2.0	44.2	24.1		
3	4.0	73.7	29.5		
4	6.0	100.1	26.4		
5	8.0	112.9	12.8		
6	10.0	122.4	9.5		
7	12.0	131.0	8.6		
8	14.0	141.2	10.2		
9	16.0	151.1	9.9		
10	18.0	159.7	8.6		
11	20.0	167.9	8.1		
12	22.0	176.8	8.9		
13	24.0	184.6	7.8		
14	26.0	192.1	7.5		
15	28.0	199.0	6.8		
C 16	30.1	207.5	8.5		
FIRST CLOSED-IN					
C 1	0.0	207.5			
2	1.0	1013.7	806.2	1.0	1.501
3	2.0	1094.8	887.3	1.9	1.201
4	3.0	1129.0	921.6	2.8	1.039
5	4.0	1150.8	943.3	3.5	0.932
6	5.0	1164.5	957.0	4.3	0.849
7	6.0	1175.7	968.3	5.0	0.780
8	7.0	1186.2	978.7	5.7	0.726
9	8.0	1194.0	986.5	6.3	0.677
10	9.0	1199.5	992.1	6.9	0.638
11	10.0	1205.8	998.3	7.5	0.604
12	12.0	1214.4	1006.9	8.6	0.546
13	14.0	1221.9	1014.4	9.5	0.499
14	16.0	1228.3	1020.8	10.4	0.460
15	18.0	1232.9	1025.5	11.3	0.427
16	20.0	1237.4	1030.0	12.0	0.399
17	22.0	1241.2	1033.7	12.7	0.374
18	24.0	1243.8	1036.3	13.4	0.353
19	26.0	1246.1	1038.7	13.9	0.334
20	28.0	1249.0	1041.5	14.5	0.317
D 21	29.0	1250.1	1042.7	14.8	0.309
SECOND FLOW					
E 1	0.0	221.8			
2	2.0	221.1	-0.7		
3	4.0	226.1	5.0		
4	6.0	233.4	7.3		
5	8.0	240.1	6.6		
6	10.0	247.4	7.3		
7	12.0	254.7	7.3		

REF	MINUTES	PRESSURE	ΔP	$\frac{t \times \Delta t}{t + \Delta t}$	$\log \frac{t + \Delta t}{\Delta t}$
SECOND FLOW - CONTINUED					
8	14.0	261.4	6.6		
9	16.0	268.2	6.8		
10	18.0	274.5	6.2		
11	20.0	280.2	5.7		
12	22.0	286.1	5.8		
13	24.0	292.4	6.3		
14	26.0	298.4	5.9		
15	28.0	303.9	5.6		
F 16	30.9	312.4	8.5		
SECOND CLOSED-IN					
F 1	0.0	312.4			
2	1.0	1032.0	719.6	1.0	1.776
3	2.0	1098.2	785.8	1.9	1.497
4	3.0	1128.9	816.5	2.9	1.327
5	4.0	1148.0	835.6	3.7	1.211
6	5.0	1161.4	848.9	4.6	1.121
7	6.0	1171.3	858.9	5.5	1.048
8	7.0	1178.7	866.2	6.3	0.989
9	8.0	1185.5	873.1	7.1	0.935
10	9.0	1191.0	878.6	7.8	0.892
11	10.0	1196.8	884.3	8.6	0.852
12	12.0	1205.1	892.6	10.0	0.785
13	14.0	1211.7	899.3	11.4	0.729
14	16.0	1217.3	904.9	12.6	0.683
15	18.0	1222.3	909.8	13.9	0.641
16	20.0	1226.6	914.2	15.0	0.608
17	22.0	1230.9	918.5	16.2	0.577
18	24.0	1233.2	920.8	17.2	0.550
19	26.0	1236.5	924.0	18.2	0.524
G 20	28.6	1239.5	927.1	19.5	0.496

REMARKS:

TICKET NO: 43656300

CLOCK NO: 7046 HOUR: 12



GAUGE NO: 7347

DEPTH: 3922.0

REF	MINUTES	PRESSURE	ΔP	$\frac{t \times \Delta t}{t + \Delta t}$	$\log \frac{t + \Delta t}{\Delta t}$
FIRST FLOW					
B 1	0.0	56.4			
2	2.0	80.5	24.2		
3	4.0	109.5	28.9		
4	6.0	135.2	25.7		
5	8.0	145.3	10.1		
6	10.0	155.3	10.1		
7	12.0	164.6	9.3		
8	14.0	174.3	9.7		
9	16.0	181.9	7.6		
10	18.0	190.5	8.6		
11	20.0	198.9	8.3		
12	22.0	206.2	7.4		
13	24.0	213.5	7.3		
14	26.0	221.3	7.8		
15	28.0	228.6	7.3		
C 16	30.1	236.2	7.6		
FIRST CLOSED-IN					
C 1	0.0	236.2			
2	1.0	1075.6	839.4	1.0	1.479
3	2.0	1130.1	893.9	1.8	1.213
4	3.0	1162.1	925.9	2.7	1.045
5	4.0	1180.7	944.6	3.5	0.934
6	5.0	1195.5	959.3	4.3	0.848
7	6.0	1206.4	970.2	5.0	0.777
8	7.0	1215.0	978.8	5.7	0.722
9	8.0	1222.2	986.0	6.3	0.678
10	9.0	1228.0	991.8	6.9	0.640
11	10.0	1233.5	997.3	7.5	0.602
12	12.0	1242.9	1006.7	8.6	0.545
13	14.0	1249.7	1013.5	9.6	0.499
14	16.0	1255.6	1019.4	10.4	0.461
15	18.0	1260.1	1023.9	11.3	0.427
16	20.0	1264.3	1028.1	12.0	0.399
17	22.0	1267.3	1031.1	12.7	0.374
18	24.0	1270.4	1034.2	13.3	0.353
19	26.0	1273.1	1036.9	14.0	0.334
20	28.0	1275.0	1038.8	14.5	0.317
D 21	29.0	1276.2	1040.0	14.8	0.309
SECOND FLOW					
E 1	0.0	255.2			
2	2.0	250.1	-5.1		
3	4.0	253.8	3.7		
4	6.0	260.8	7.1		
5	8.0	268.3	7.5		
6	10.0	275.4	7.1		
7	12.0	281.3	5.9		

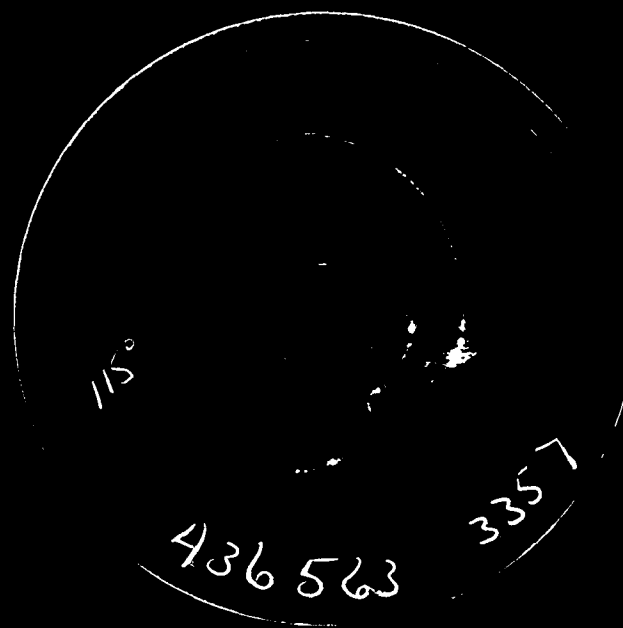
REF	MINUTES	PRESSURE	ΔP	$\frac{t \times \Delta t}{t + \Delta t}$	$\log \frac{t + \Delta t}{\Delta t}$
SECOND FLOW - CONTINUED					
8	14.0	288.4	7.2		
9	16.0	295.2	6.8		
10	18.0	301.9	6.7		
11	20.0	307.5	5.6		
12	22.0	313.9	6.4		
13	24.0	320.2	6.3		
14	26.0	326.3	6.1		
15	28.0	332.1	5.8		
F 16	30.9	340.4	8.3		
SECOND CLOSED-IN					
F 1	0.0	340.4			
2	1.0	1072.0	731.6	1.0	1.790
3	2.0	1136.2	795.7	1.9	1.503
4	3.0	1165.1	824.7	2.8	1.331
5	4.0	1182.8	842.3	3.7	1.212
6	5.0	1195.4	855.0	4.6	1.119
7	6.0	1204.9	864.5	5.5	1.047
8	7.0	1212.5	872.1	6.3	0.989
9	8.0	1219.0	878.6	7.0	0.938
10	9.0	1224.2	883.8	7.8	0.892
11	10.0	1229.7	889.2	8.6	0.850
12	12.0	1236.3	895.8	10.0	0.785
13	14.0	1242.4	902.0	11.4	0.729
14	16.0	1247.8	907.3	12.7	0.683
15	18.0	1252.2	911.8	13.9	0.642
16	20.0	1256.0	915.6	15.0	0.608
17	22.0	1259.0	918.6	16.1	0.577
18	24.0	1261.6	921.2	17.2	0.549
19	26.0	1263.9	923.5	18.2	0.525
G 20	28.6	1266.8	926.3	19.5	0.496

REMARKS:

		O.D.	I.D.	LENGTH	DEPTH
1		4.500	3.826	3631.0	
3		6.250	2.250	89.0	
50		6.000	2.750	1.0	3720.0
3		6.250	2.250	119.0	
5		6.000	2.250	1.0	
12		5.750	0.870	6.0	
60		5.000	0.750	5.0	3851.0
80		5.000	2.250	4.0	3853.0
15		5.000	1.750	5.0	
16		5.000	1.000	3.0	
70		6.750	1.530	6.0	3868.0
70		6.750	1.530	6.0	3874.0
5		6.000	2.250	1.0	
3		6.250	2.250	31.0	
5		6.000	2.250	1.0	
5		6.000	2.250	1.0	
20		5.000	2.370	10.0	
83		5.000		1.0	3920.0
81		5.000		4.0	3922.0
TOTAL DEPTH					3925.0

EQUIPMENT DATA

TEMPERATURE RECORDER CHART



10° each circle

EQUATIONS FOR DST GAS WELL ANALYSIS

Indicated Flow Capacity	$kh = \frac{.001637 Q_g T}{m}$	md-ft
Average Effective Permeability	$k = \frac{kh}{h}$	md
Skin Factor	$S = 1.151 \left[\frac{m(P^*) - m(P_i)}{m} - \text{LOG} \left(\frac{k (t/60)}{\phi \mu c_i r_w^2} \right) + 3.23 \right]$	
Damage Ratio	$DR = \frac{m(P^*) - m(P_i)}{m(P^*) - m(P_i) - 0.87 mS}$	
Indicated Flow Rate (Maximum)	$AOF_1 = \frac{Q_g m(P^*)}{m(P^*) - m(P_i)}$	MCFD
Indicated Flow Rate (Minimum)	$AOF_2 = Q_g \sqrt{\frac{m(P^*)}{m(P^*) - m(P_i)}}$	MCFD
Approx. Radius of Investigation	$r_i = 0.032 \sqrt{\frac{k (t/60)}{\phi \mu c_i}}$	ft