Form G-2
(Rev. 1/03)

KANSAS CORPORATION COMMISSION
ONE POINT STABILIZED OPEN FLOW OR DELIVERABILITY TEST

Type Test: Open Flow / Deliverabilty *(See Instructions on Reverse Side)*

Test Date: 6/20/2002	API No. 15: 023-20438-00-00		
Company: NOBLE ENERGY INC.	Lease: SCHLEPP	Well Number: 24-29	
County: CHEYENNE	Location: SESW/4	Section: 29	TWP: 3S
RNG (E/W): 41W	Acres Attributed: 160		
Field: CHERRY CREEK	Reservoir: NIOBRARA	Gas Gathering Connection: BITTER CREEK PIPELINE	
Completion Date: 6/17/02	Plug Back Total Depth: 1634	Packer Set at:	
Casing Size: 4 1/2	Weight: 10.5#	Internal Diameter: 4.052"	Set at: 1658
Perforations: 1484	To: 1524		
Tubing Size:	Weight:	Internal Diameter:	Set at:
Perforations:	To:		
Type Completion (Describe): SINGLE (GAS)	Type Fluid Production:	Pump Unit or Traveling Plunger? Yes / (No)	
Producing Thru (Annulus / Tubing): CASING	% Carbon Dioxide: —	% Nitrogen: —	Gas Gravity - G_g: 0.6
Vertical Depth(H): 1524	Pressure Taps: Flange	(Meter Run) (Prover) Size: 2"	

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Pressure Buildup: Shut in _____ 19 ___ at _____ (AM) (PM) Taken 6/20/02 at _____ (AM) (PM)

Well on Line: Started 6/26/02 at 11:30 (AM) (PM) Taken _____ 19 ___ at _____ (AM) (PM)

OBSERVED SURFACE DATA

Duration of Shut-in _____ Hours

Static / Dynamic Property	Orifice Size inches	Circle one: (Meter or) Prover Pressure psig	Pressure Differential in (h) Inches H_2O	Flowing Temperature t	Well Head Temperature t	Casing Wellhead Pressure (P_w) or (P_t) or (P_c) psig	Casing psia	Tubing Wellhead Pressure (P_w) or (P_t) or (P_c) psig	Tubing psia	Duration (Hours)	Liquid Produced (Barrels)
Shut-In						254	267	NA	NA	—	—
Flow	3/8	86	145	64.5		86	99	NA	NA	24	0

FLOW STREAM ATTRIBUTES

Plate Coeffiecient (F_b) (F_p) Mcfd	Circle one: (Meter) or Prover Pressure psia	Press Extension $\sqrt{P_m \times H_w}$	Gravity Factor F_g	Flowing Temperature Factor F_{tt}	Deviation Factor F_{pv}	Metered Flow R (Mcfd)	GOR (Cubic Feet/ Barrel)	Flowing Fluid Gravity G_m
0.6860	100.4	120.66	1.291	0.9867	1.000	105		

(OPEN FLOW) (DELIVERABILITY) CALCULATIONS

$(P_c)^2$ = 72.0 : $(P_w)^2$ = 10.08 : P_d = _____ % $(P_c - 14.4) + 14.4$ = _____ : $(P_a)^2$ = 0.207 $(P_d)^2$ = _____

$(P_c)^2 - (P_a)^2$ or $(P_c)^2 - (P_d)^2$	$(P_c)^2 - (P_w)^2$	Choose formula 1 or 2: 1. $P_c^2 - P_a^2$ 2. $P_c^2 - P_d^2$ divided by: $P_c^2 - P_w^2$	LOG of formula 1. or 2. and divide by: $P_c^2 - P_w^2$	Backpressure Curve Slope = "n" or Assigned Standard Slope	n x LOG	Antilog	Open Flow Deliverability Equals R x Antilog Mcfd
71.79	61.92	1.1594	0.0642	0.87	0.0559	1.1373	119.9

Open Flow 120 Mcfd @ 14.65 psia Deliverability 101 Mcfd @ 14.65 psia

The undersigned authority, on behalf of the Company, states that he is duly authorized to make the above report and that he has knowledge of the facts stated therein, and that said report is true and correct. Executed this the 2 day of APR, 19 03.

Witness (if any)

For Company

For Commission

Checked by

Schlepp 24-29
- first 24 hours flow data into pipeline
- data used as "one point"

Date	Total Flow MCFD	Hrs On	DP_Avg	SP_Avg	PT_Avg
6/27/2002	101	24.0	145.019 InH2O	85.8728 psi	64.4668 DegF