## KANSAS CORPORATION COMMISSION ONE POINT STABILIZED OPEN FLOW OR DELIVERABILITY TEST

Type Tes	st:					(	(See Instru	uctions on Re	verse Side	9)					
✓ Open Flow															
✓ Deliverabilty						Test Date: 11/11 to 11/12/10				API No. 15 007-23,376 <b>1200</b>					
Company HermanL. Loeb, LLC							Lease Cinda/Lytle				5			Well Number	
County Location Barber SESESW					Section 12		TWP			/W)	Acres Attributed				
Field						Reservoir			Gas Gathering Connec						
Completion Date 2/23/09					Plug Bac	Plug Back Total Depth			Packer						
Casing Size Weight						4924 Internal [	Diameter		Set at Perforations			То			
5.5 Tubing Size Weight					Internal [	Diameter	Set a	4966         4464           Set at         Perforation			4512 To				
2.375 Type Completion (Describe)						Type Flui	4618 Type Fluid Production			Pump U	g Plunger? Yes	/ No			
single Producing Thru (Annulus / Tubing)						Öil & S	Öil & SW			Yes -	pumping u	nit			
annulus					.094	% Carbon Dioxide .094			% Nitrog 2.772		Gas Gravity - G <sub>g</sub> .706				
Vertical Depth(H)						Pressure Taps flange					•	(Meter Run) (Prover) Size 2"			
11/08 10 9:30 am 11/11 10 9:30 am												(AM) (PM)			
11/11 10 9:30 am 11/12 10 9:30 am											(AM) (PM)				
							OBSERV	ED SURFACE	E DATA		***	Duration of Shu	t-in 72	Hours	
Static / Dynamic Property	Dynamic Size		Circle one:  Meter Prover Pressure psig (Pm)		Pressure Differential in Inches H <sub>2</sub> 0	Flowing Well Hear Temperature t		(P <sub>w</sub> ) or (P <sub>t</sub> ) or (P <sub>c</sub> )		Tubing Wellhead Pressure $(P_w)$ or $(P_t)$ or $(P_c)$		Duration (Hours)	Liqu	Liquid Produced (Barrels)	
Shut-In	hut-In		paig (i		Inches H <sub>2</sub> O			267	281.4	psig	psia	72			
Flow	Flow 1.000		30		12.1	50		245	259.4			24			
							FLOW ST	REAM ATTRI	BUTES						
Plate Coeffiecient (F <sub>b</sub> ) (F <sub>p</sub> ) Mcfd			Circle one: Meter or Prover Pressure psia		Press Grav Extension Fact  ✓ P <sub>m</sub> xh F <sub>g</sub>		or Temperature		Deviation Factor F <sub>pv</sub>		Metered Flo R (Mcfd)	w GOR (Cubic F Barrel	eet/	Flowing Fluid Gravity G <sub>m</sub>	
5.073	5.073 4		4.4 2		23.18	1.190	) 1	.010			141			.706	
$(P_c)^2 = _{_{_{_{_{c}}}}} 7$	9.18	<b>5</b> :	(P <sub>w</sub> )	6	7.288 :	(OPEN FLO		<b>VERABILITY)</b> _% (P	CALCULA - 14.4) +		:		) <sup>2</sup> = 0.2	207	
$(P_c)^2 - (P_a)^2$ or $(P_c)^2 - (P_d)^2$		(P <sub>c</sub> ) <sup>2</sup> - (P <sub>w</sub> ) <sup>2</sup>		Cho	ose formula 1 or 2: 1. $P_c^2 - P_a^2$ 2. $P_c^2 - P_d^2$ led by: $P_c^2 - P_w^2$	LOG of formula 1. or 2. and divide	formula 1. or 2. and divide p 2 p 2		Backpressure Curve Slope = "n" or Assigned Standard Slope		og [	Antilog	O De Equals	Open Flow Deliverability Equals R x Antilog (Mcfd)	
78.97	8	11	.897	6.	638	.8220		.653		.53	67	3.44	485	5	
Open Flow 485 Mcfd @ 14.65 psia X .							50 =	Deliverability 242.5			Mcfd @ 14.65 psia				
									•		_	ort and that he ha			
the facts st	tated t	herein	, and that	said	report is true	and correct	. Executed	d this the 12	<u>ui</u> d	ay of N	ovember		,	20 10 .	
Witness (if any)									-/-	el m, i	For C	Company	REC	EIVED	
			For Cor	nmissio	n						Chec	cked by	NON	1 5 2010	