The second

KANSAS CORPORATION COMMISSION ONE POINT STABILIZED OPEN FLOW OR DELIVERABILITY TEST

Type Test	t:				(See Instruct	ions on Reve	rse Side	e)				
Open Flow Deliverability			Test Date:			API No. 15							
De	liverab	ilty	• **		10/05				15-0	07-22816	<u>-0000</u>		
Company JACK EX		RAT	ION, INC.		ð		Lease BENSON				3-4	Well Num	nber
County Location BARBER NW SE NE			Section TWP 04 35S				RNG (E/V 14W	V)		Acres Attributed			
Field AETNA	SE				Reservoir	SIPPIAN				ering Conne	ection		
Completic 06/15/20		е	,		Plug Bac 5004	k Total Dept	th		Packer Se	et at			
Casing S 4.5	ize		Weight		Internal 0 4.0	Diameter	Set at 5009			Perforations To 4826 4905			
Tubing Size Weight 2.375 4.7				Internal Diameter Set at 1.995				Perforations					
Type Con		n (D	escribe)		Type Flui WATE	d Production	า			t or Traveling ER LIFT	Plunger? Yes	/ No	
Producing		(Anı	nulus / Tubing)	% C	Carbon Dioxi	de		% Nitroge	n	Gas G	ravity - G	,
Vertical D	epth(F	1)	· · · · · · · · · · · · · · · · · · ·			Pres	sure Taps			- controller	(Meter	Run) (Pro	over) Size
Pressure	Buildu	p :	Shut in 09/	′02 2	0_10 _{at}		(AM) (PM) T	aken		20	at	(A	(M) (PM)
Well on L	.ine:		Started 10								at		
			.	1		OBSERVE	D SURFACE		Т		Duration of Shut	-in	Hours
Static / Dynamic Property	Dynamic Size		Meter Differential . Prover Pressure in		Flowing Well Head Temperature t t		Casing Wellhead Pressure (P_w) or (P_t) or (P_c)		Tubing Wellhead Pressure $(P_w) \text{ or } (P_1) \text{ or } (P_c)$		Duration Li (Hours)		Produced arrels)
Shut-In			psig (Pm) Inches H ₂ 0			psig psia		أماله يو	psig psla		-75		
Flow													
	I					FLOW STR	REAM ATTRIE	UTES					
Plate Coeffiecient (F _b) (F _p) Mcfd		Pro	Circle one: Meter or over Pressure psia	Press Extension P _m x h	ion Factor		Flowing Temperature Factor F ₁₁	Fa	riation actor F _{pv}	Metered Flow GOP R (Cubic F (Mcfd) Barre		eet/	Flowing Fluid Gravity G _m
(P) ² =		:	(P _w) ² =	:	,	• •	'ERABILITY)			:) ² = 0.20) ² =	17
$(P_c)^2 = {(P_c)^2 - (P_g)^2}$ or $(P_c)^2 - (P_d)^2$			$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$		Backpressure Curve		e n x L	Γ٦	Antilog	Open Flo Deliverabi Equals R x A (Mctd)			
Open Flo	w			Mcfd @ 14.	65 psia		Deliverabil	ity			Mcfd @ 14.65 p	sia	
		igne	d authority, or	behalf of the	Company,	states that h	ne is duly aut	horized	to make the	above repo	rt and that he h	as knowle	edge of
the facts s	stated t	here	in, and that sa	id report is true	e and correc	ct. Executed	this the 4T	H	day of N	OVEMBER		, 2	.0 10 .
			110-					A W Ter-E1			Company	RE	CEIVED
			Witness (i			,						NO1	1 2 2 20
			For Comm	ission						Che	cked by		

exempt status und	er penalty of perjury under the laws of the state of Kansas that I am authorized to request er Rule K.A.R. 82-3-304 on behalf of the operator <u>JACK EXPLORATION</u> , INC.
correct to the best of equipment insta I hereby reque	oing pressure information and statements contained on this application form are true and of my knowledge and belief based upon available production summaries and lease records llation and/or upon type of completion or upon use being made of the gas well herein named. est a one-year exemption from open flow testing for the BENSON 3-4 punds that said well:
	is a coalbed methane producer is cycled on plunger lift due to water is a source of natural gas for injection into an oil reservoir undergoing ER is on vacuum at the present time; KCC approval Docket No. is not capable of producing at a daily rate in excess of 250 mcf/D to supply to the best of my ability any and all supporting documents deemed by Commission to corroborate this claim for exemption from testing.
	Signature: <u>Seley Carow</u> Title: <u>SECRETARY</u>

Instructions:

If a gas well meets one of the eligibility criteria set out in KCC regulation K.A.R. 82-3-304, the operator may complete the statement provided above in order to claim exempt status for the gas well.

At some point during the current calendar year, wellhead shut-in pressure shall have been measured after a minimum of 24 hours shut-in/buildup time and shall be reported on the front side of this form under **OBSERVED SURFACE DATA**. Shut-in pressure shall thereafter be reported yearly in the same manner for so long as the gas well continues to meet the eligibility criterion or until the claim of eligibility for exemption **IS** denied.

The G-2 form conveying the newest shut-in pressure reading shall be filed with the Wichita office no later than December 31 of the year for which it's intended to acquire exempt status for the subject well. The form must be signed and dated on the front side as though it was a verified report of annual test results.

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JACK EXPLORATION, INC. **R/D Property Volume Analysis Report By Sales Date from 8/1/2009 to 9/30/2010

For All Leases and Selected Wells

			****** GRC)\$\$******	******* SHARE ******		
	Production Date	Sale Date	Sales Volume	Prod Volume	Sales Volume	Prod Volume	
Lease: SLT Well: SLT08 Ref #: 00000018			Well Name: Ber	ison 3-4			
Account:	361-01	Department:	Ac	count Name: DRY	'GAS		
	8/31/2009	8/31/2009	1,516.55	1,688.97	1,516.55	1,688.97	
	10/31/2009	10/31/2009	2,150.05	2,394.48	2,150.05	2,394.48	
	11/30/2009	11/30/2009	1,558.72	1,735.93	1,558.72	1,735.93	
	12/31/2009	12/31/2009	1,550.70	1,727.00	1,550.70	1,727.00	
	1/31/2010	1/31/2010	1,440.63	1,615.95	1,440.63	1,615.95	
	2/28/2010	2/28/2010	1,268.04	1,422.35	1,268.04	1,422.35	
	3/31/2010	3/31/2010	1,352.97	1,517.62	1,352.97	1,517.62	
	4/30/2010	4/30/2010	1,288.91	1,444.80	1,288.91	1,444.80	
	5/31/2010	5/31/2010	1,308.13	1,466.34	1,308.13	1,466.34	
	6/30/2010	6/30/2010	1,258.52	1,410.73	1,258.52	1,410.73	
	7/31/2010	7/31/2010	728.04	816.09	728.04	816.09	
	8/31/2010	8/31/2010	500.13	560.62	500.13	560.62	
		•	15,921.39	17,800.88	15,921.39	17,800.88	
Property Totals			15,921.39	17,800.88	15,921.39	17,800.88	
	Report	t Totals	15,921.39	17,800.88	15,921.39	17,800.88	

yand

Date: 11/4/2010

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Atlas Pipeline Company

Analysis

July, 2010

, Avard System									
Meter Number:	95242069	Meter Name:	Benso	on 3-4					
Relative Density:	0.650	C2+ GPM:	2	2.9118	Wet Heating Value:	1107.5			
Pressure Base:	14.730	C5+ GPM:		0.2746	Dry Heating Value:	1127.1			
		C6+ GPM:			As Del Heating Value:	1092.2			
Temperature Base:	60.00	Co+ GPM.		J. 1440	, to bot floating value.	1002.2			
			Mol %	GPM					
		Carbon Dioxide	0.081	0.0137	•				
		Nitrogen	2.013	0.2214					
		Methane	87.602	14.8474					
		Ethane	6.034	1.6133					
		Propane	2.565	0.7066					
		Iso-Butane	0.275	0.0901					
		N-Butane	0.721	0.2272					
		Iso-Pentane	0.157	0.0576	•				
		N-Pentane	0.199	0.0722	•				
		Hexane	0.352	0.1448					
		Heptane							
		Octane							
		Nonanė							
		Decane				•			
		Oxygen		ı					
	· · · · · · · · · · · · · · · · · · ·	Hydrogen							
		Helium	•						
		Argon							
		Water Vapor							
		Hydrogen Sulfide							
		Total	100.000	17.9943					
		- 	_						

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APLMC WestOk

GAS VOLUME STATEMENT

CLOSED DATA

Avard System

95242069 --- Benson 3-4 July, 2010

Measured Conditions

Meter Status: In Service

Pressure Base: 14.730 psia

CO2

H2O

2.53

1.42

16.64

10.55

Temperature Base:

60.00 °F

He

HV Cond: Wet

Meter Type: EFM

Contract Hr.: Midnight

Water Vapor Corr. Technique:

H2S 02

C1 87.602

C2 6.034

Plate

(inches)

1.000

1.000

1.000

1.000

1.000

1.000

1.000

1.000

1.000

1 000

1.000

1.000

1.000

1.000

1.000

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1.000

1.000

1.000

1.000

1.000

1.000 1.000

1.000

1.000

1.000

1.000

I-C4 C3 0.275 2.565

Volume

(Mcf)

41.53

41.33

41.48

41.51

38.57

34.35

14.69

0.00

38.10

29.71

19.18

16.47

6.77

27.94

24.83

20.07

18.57

19.61

10.70

28.27

21.98

8.47

7.64

34.46

25.51

20.79

19.91

13.66

17.24

31.95

8.80

724.09

N-C4

I-C5 N-C5 C6+

3/4/10

0.081 2.013 Tube I.D.

N2

Tap Location interval 1 Hour

- Tap Type Flange

0.6499

0.6499

0.6499

0.6499

0.6499

0.6499

11.50

9.84

6.13

7 43

Atmos. Pressure 13.800 psi

Water Vapor Corr. Method:

0.721 Calc. Method

AGA3-1992

Heating Value

(BTU/scf)

1107.46

1107.46

1107.46

1107.46

1107.46

1107 46

1107.46

1107.46

1107.46

1107.46

1107.46

1107.46

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1107.46

0.157 0.199 **Fpv Method**

AGA8-Detail

46.00

45.77

45.94

45.97

42.72

38 04

16.27

0.00

42.20

32.90

21 24

18.24

7.49

30.94

27.49

22.23

20.57

21.72

11.85

31.30

24.34

9.38

8.46

38 16

28.25

23.02

22.05

15.12

19 09

35.39

9.74

801.90

Energy

(MMBTU)

0.352 Sample Date

2.072 in.

10

11

20

30

31

TOTAL

Upstream Hours Differential Pressure Temperature

Relative (In. H2O) (PSIA) (°F) Flow Density Day 2.88 0.6499 71.90 46.85 81.05 1 2.80 0.6499 2 74.15 47.55 78.92

76.35 45.27 77.37 2.85 0.6499 3 2.84 0.6499 77.44 4 78.13 44.57 62.05 45.88 72.76 4.62 0.6499 12.51 0.6499 84.12 6 14.24 42.20 7 2.90 40.42 77.66 5.26 0.6499 75.86 0.00 0.6499 8 0.00 40.81 9.58 0.6499 9 17.74 46.80 89.18

42.76

41.95

82.42

89.46

87.69

83.75

8 21 0.6499 12 1.47 43.10 86.26 75.62 2.97 0.6499 13 1.84 41.68 4.78 0.6499 22 70 50.33 98.30 14 5.93 0.6499 6.92 42.93 87.00 15 5.15 0.6499 16 6.11 42.30 91.66 5.13 0.6499 93 01 17 5.05 42.51 93.15 5.31 0.6499 18 6.74 42.41 88.59 2.36 75.92 49.51 19

44.77

6.13 0.6499 21 6.47 41.58 90.18 2.86 0.6499 22 3.49 40.80 82 71 0.6499 229.64 96.60 0.22 23 78.09 83.25 5.35 0.6499 69.95 50.44 24 6.78 0.6499 25 18.69 42.44 79.58 26 17.80 46.10 84.42 5.62 0.6499 0.6499 6.67 27 3.39 42.15 86.43 0.6499 28 55.32 46.26 81.70 2.95 0.6499 86.91 1,43 54.74 29 50.42

42.83

2.93 3.63 41.87 78.36 159.05 84.09 35.85 45.23 Volume at 14.650 = 728.04 Energy = 801.90

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