Form G-2
(Rev. 7/03)

KANSAS CORPORATION COMMISSION
ONE POINT STABILIZED OPEN FLOW OR DELIVERABILITY TEST

(See Instructions on Reverse Side)

Type Test:
- [x] Open Flow
- [ ] Deliverabilty

Test Date: 10/05/2010

API No. 15: 15-007-22920-00-00

Company	Lease	Well Number
JACK EXPLORATION, INC.	BENSON	2-33

County	Location	Section	TWP	RNG (E/W)	Acres Attributed
BARBER	E/2 W/2 NE	33	34S	14W	320

Field	Reservoir	Gas Gathering Connection
AETNA SE	MISSISSIPPIAN	ATLAS PIPELINE

Completion Date	Plug Back Total Depth	Packer Set at
11/23/2005	5150	

Casing Size	Weight	Internal Diameter	Set at	Perforations	To
4.5	11.6	4.0	5169	4898-4918	4922-5002

Tubing Size	Weight	Internal Diameter	Set at	Perforations	To
2.375	4.7	1.995	4886.38		

Type Completion (Describe)	Type Fluid Production	Pump Unit or Traveling Plunger? Yes / No
SINGLE	WATER	PLUNGER LIFT

Producing Thru (Annulus / Tubing)	% Carbon Dioxide	% Nitrogen	Gas Gravity - G_g
TUBING			

Vertical Depth(H)	Pressure Taps	(Meter Run) (Prover) Size
	FLANGE	

Pressure Buildup: Shut in 09/01 20 10 at _____ (AM) (PM) Taken _____ 20 ___ at _____ (AM) (PM)

Well on Line: Started 10/06 20 10 at _____ (AM) (PM) Taken _____ 20 ___ at _____ (AM) (PM)

OBSERVED SURFACE DATA Duration of Shut-in _____ Hours

Static / Dynamic Property	Orifice Size (inches)	Circle one: Meter Prover Pressure psig (Pm)	Pressure Differential in Inches H_2O	Flowing Temperature t	Well Head Temperature t	Casing Wellhead Pressure (P_w) or (P_t) or (P_c) psig	Casing Wellhead Pressure (P_w) or (P_t) or (P_c) psia	Tubing Wellhead Pressure (P_w) or (P_t) or (P_c) psig	Tubing Wellhead Pressure (P_w) or (P_t) or (P_c) psia	Duration (Hours)	Liquid Produced (Barrels)
Shut-In							350		350		
Flow											

FLOW STREAM ATTRIBUTES

Plate Coeffiecient (F_b) (F_p) Mcfd	Circle one: Meter or Prover Pressure psia	Press Extension $\sqrt{P_m x h}$	Gravity Factor F_g	Flowing Temperature Factor F_{ft}	Deviation Factor F_{pv}	Metered Flow R (Mcfd)	GOR (Cubic Feet/ Barrel)	Flowing Fluid Gravity G_m

(OPEN FLOW) (DELIVERABILITY) CALCULATIONS

$(P_a)^2$ = 0.207

$(P_c)^2$ = _____ : $(P_w)^2$ = _____ : P_d = _____ % $(P_c - 14.4) + 14.4$ = _____ : $(P_d)^2$ = _____

$(P_c)^2 - (P_a)^2$ or $(P_c)^2 - (P_d)^2$	$(P_c)^2 - (P_w)^2$	Choose formula 1 or 2: 1. $P_c^2 - P_a^2$ 2. $P_c^2 - P_d^2$ divided by: $P_c^2 - P_w^2$	LOG of formula 1. or 2. and divide by: $P_c^2 - P_w^2$	Backpressure Curve Slope = "n" or Assigned Standard Slope	n x LOG	Antilog	Open Flow Deliverability Equals R x Antilog (Mcfd)

Open Flow _____ Mcfd @ 14.65 psia Deliverability _____ Mcfd @ 14.65 psia

The undersigned authority, on behalf of the Company, states that he is duly authorized to make the above report and that he has knowledge of the facts stated therein, and that said report is true and correct. Executed this the 4TH day of NOVEMBER, 20 10.

Witness (if any)

For Company

For Commission

Checked by

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NOV 22 2010
KCC WICHITA

Form G-2
(Rev. 7/03)

I declare under penalty of perjury under the laws of the state of Kansas that I am authorized to request exempt status under Rule K.A.R. 82-3-304 on behalf of the operator JACK EXPLORATION, INC. and that the foregoing pressure information and statements contained on this application form are true and correct to the best of my knowledge and belief based upon available production summaries and lease records of equipment installation and/or upon type of completion or upon use being made of the gas well herein named.

I hereby request a one-year exemption from open flow testing for the BENSON 2-33 gas well on the grounds that said well:

(Check one)

- [ ] is a coalbed methane producer
- [x] is cycled on plunger lift due to water
- [ ] is a source of natural gas for injection into an oil reservoir undergoing ER
- [ ] is on vacuum at the present time; KCC approval Docket No. _____
- [x] is not capable of producing at a daily rate in excess of 250 mcf/D

I further agree to supply to the best of my ability any and all supporting documents deemed by Commission staff as necessary to corroborate this claim for exemption from testing.

Date: 11/04/2010

Signature: Kelly Aaron

Title: SECRETARY

Instructions: If a gas well meets one of the eligibility criteria set out in KCC regulation K.A.R. 82-3-304, the operator may complete the statement provided above in order to claim exempt status for the gas well.

At some point during the current calendar year, wellhead shut-in pressure shall have been measured after a minimum of 24 hours shut-in/buildup time and shall be reported on the front side of this form under **OBSERVED SURFACE DATA**. Shut-in pressure shall thereafter be reported yearly in the same manner for so long as the gas well continues to meet the eligibility criterion or until the claim of eligibility for exemption **IS** denied.

The G-2 form conveying the newest shut-in pressure reading shall be filed with the Wichita office no later than December 31 of the year for which it's intended to acquire exempt status for the subject well. The form must be signed and dated on the front side as though it was a verified report of annual test results.

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JACK EXPLORATION, INC.
R/D Property Volume Analysis Report
By Sales Date from 8/1/2009 to 9/30/2010

Date: 11/4/2010

For All Leases and Selected Wells

	Production Date	Sale Date	******* GROSS ******* Sales Volume	Prod Volume	******* SHARE ******* Sales Volume	Prod Volume
Lease: SLT	**Well: SLT10**		**Well Name: Benson 2-33**			
Ref #: 00000018						
Account:	**361-01**	**Department:**		**Account Name: DRY GAS**		
	8/31/2009	8/31/2009	1,899.51	2,069.43	1,899.51	2,069.43
	10/31/2009	10/31/2009	2,498.65	2,722.16	2,498.65	2,722.16
	11/30/2009	11/30/2009	1,822.61	1,985.65	1,822.61	1,985.65
	12/31/2009	12/31/2009	622.16	677.81	622.16	677.81
	1/31/2010	1/31/2010	1,385.72	1,509.68	1,385.72	1,509.68
	2/28/2010	2/28/2010	480.61	523.60	480.61	523.60
	3/31/2010	3/31/2010	1,177.25	1,282.56	1,177.25	1,282.56
	4/30/2010	4/30/2010	1,209.72	1,320.80	1,209.72	1,320.80
	5/31/2010	5/31/2010	1,293.58	1,412.37	1,293.58	1,412.37
	6/30/2010	6/30/2010	1,242.48	1,356.57	1,242.48	1,356.57
	7/31/2010	7/31/2010	1,256.97	1,372.40	1,256.97	1,372.40
	8/31/2010	8/31/2010	646.66	706.04	646.66	706.04
			15,535.92	16,939.07	15,535.92	16,939.07
	Property Totals		15,535.92	16,939.07	15,535.92	16,939.07
	Report Totals		15,535.92	16,939.07	15,535.92	16,939.07

4.7 MCF

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Atlas Pipeline Company

Analysis

July, 2010

Avard System

Meter Number: 95242334 **Meter Name:** Benson 2-33

Relative Density:	0.622	C2+ GPM:	2.0551	Wet Heating Value:	1078.7
Pressure Base:	14.730	C5+ GPM:	0.2344	Dry Heating Value:	1097.8
Temperature Base:	60.00	C6+ GPM:	0.1283	As Del Heating Value:	1064.1

	Mol %	GPM
Carbon Dioxide	0.071	0.0120
Nitrogen	1.196	0.1315
Methane	91.507	15.5093
Ethane	4.255	1.1377
Propane	1.651	0.4548
Iso-Butane	0.212	0.0695
N-Butane	0.504	0.1588
Iso-Pentane	0.130	0.0473
N-Pentane	0.162	0.0587
Hexane	0.312	0.1283
Heptane		
Octane		
Nonane		
Decane		
Oxygen		
Hydrogen		
Helium		
Argon		
Water Vapor		
Hydrogen Sulfide		
Total	100.000	17.7080

APLMC WestOk

GAS VOLUME STATEMENT

CLOSED DATA

Avard System

95242334 --- Benson 2-33

July, 2010

Measured Conditions

Meter Status: In Service

Pressure Base: 14.730 psia **Temperature Base:** 60.00 °F **HV Cond:** Wet **Meter Type:** EFM **Contract Hr.:** Midnight

Water Vapor Corr. Technique: **Water Vapor Corr. Method:**

CO2	N2	H2O	H2S	O2	He	C1	C2	C3	I-C4	N-C4	I-C5	N-C5	C6+
0.071	1.196					91.507	4.255	1.651	0.212	0.504	0.130	0.162	0.312

Tube I.D.	Interval	Tap Location	Tap Type	Atmos. Pressure	Calc. Method	Fpv Method	Sample Date
2.070 in.	1 Hour	Upstream	Flange	13.800 psi	AGA3-1992	AGA8-Detail	3/4/10

Day	Differential (In. H2O)	Pressure (PSIA)	Temperature (°F)	Hours Flow	Relative Density	Plate (inches)	Volume (Mcf)	Heating Value (BTU/scf)	Energy (MMBTU)
1	14.25	44.16	81.34	8.57	0.6223	1.000	38.34	1078.69	41.35
2	13.07	44.12	78.06	9.20	0.6223	1.000	42.69	1078.69	46.05
3	11.42	41.79	77.62	8.19	0.6223	1.000	37.29	1078.69	40.23
4	12.96	40.94	76.64	9.49	0.6223	1.000	44.29	1078.69	47.78
5	17.65	42.91	72.12	7.90	0.6223	1.000	36.60	1078.69	39.48
6	23.10	42.98	77.25	9.49	0.6223	1.000	44.04	1078.69	47.51
7	21.58	42.82	78.14	7.97	0.6223	1.000	38.15	1078.69	41.15
8	13.84	42.96	76.58	9.42	0.6223	1.000	42.45	1078.69	45.79
9	16.92	44.72	79.81	8.34	0.6223	1.000	40.58	1078.69	43.77
10	15.65	44.06	82.17	9.06	0.6223	1.000	40.17	1078.69	43.33
11	22.39	43.86	85.96	8.70	0.6223	1.000	41.49	1078.69	44.75
12	21.00	45.19	84.38	8.69	0.6223	1.000	38.74	1078.69	41.78
13	21.21	44.27	85.35	9.07	0.6223	1.000	42.80	1078.69	46.17
14	15.30	46.38	88.14	8.33	0.6223	1.000	37.60	1078.69	40.56
15	18.60	43.79	83.18	9.44	0.6223	1.000	43.25	1078.69	46.66
16	18.57	43.74	88.41	7.96	0.6223	1.000	36.42	1078.69	39.29
17	15.97	43.84	89.02	9.49	0.6223	1.000	43.39	1078.69	46.81
18	16.60	43.36	90.46	7.91	0.6223	1.000	36.39	1078.69	39.25
19	14.24	46.87	89.26	9.50	0.6223	1.000	44.03	1078.69	47.49
20	15.04	45.61	88.79	8.18	0.6223	1.000	39.83	1078.69	42.96
21	11.74	42.25	89.00	9.22	0.6223	1.000	40.91	1078.69	44.13
22	14.55	41.99	88.17	8.54	0.6223	1.000	41.24	1078.69	44.48
23	12.68	42.48	89.27	8.85	0.6223	1.000	39.47	1078.69	42.58
24	13.99	42.96	83.48	8.92	0.6223	1.000	41.87	1078.69	45.17
25	16.65	42.32	78.80	8.48	0.6223	1.000	37.78	1078.69	40.75
26	23.00	45.37	83.00	9.28	0.6223	1.000	42.77	1078.69	46.14
27	23.12	44.00	84.58	8.12	0.6223	1.000	36.71	1078.69	39.60
28	19.42	43.42	84.10	9.49	0.6223	1.000	43.45	1078.69	46.87
29	19.23	43.66	86.48	7.91	0.6223	1.000	36.42	1078.69	39.29
30	14.82	52.43	87.11	9.51	0.6223	1.000	43.59	1078.69	47.02
31	17.19	55.05	88.05	8.00	0.6223	1.000	37.41	1078.69	40.35
TOTAL	16.95	44.33	83.68	271.20	0.6223		1,250.14		1,348.52

Volume at 14.650 = 1,256.97 Energy = 1,348.52

40mcf