

KANSAS CORPORATION COMMISSION ONE POINT STABILIZED OPEN FLOW OR DELIVERABILITY TEST

Type Test:

(See Instructions on Reverse Side)

- Open Flow
 Deliverability

Test Date:
6/9/11

API No. 15
-185-23174-00-00

| | | | | | |
|--|-----------------------|--------------------------------|-----------------|--|-------------------------|
| Company Becker Oil Corporation | | Lease McCune | | Well Number 1 A | |
| County Stafford | Location E/2 SW NE | Section 12 | TWP 25S | RNG (E/W) 13W | Acres Attributed 640 |
| Field Leesburg North | | Reservoir Chase Group | | Gas Gathering Connection ONEOK | |
| Completion Date 3/24/03 | | Plug Back Total Depth 2008' | | Packer Set at | |
| Casing Size 4 1/2" | Weight 10.5# | Internal Diameter 4.052 | Set at 3020' | Perforations 1965 | To 1985 |
| Tubing Size 2 3/8" | Weight 4.7# | Internal Diameter 2" | Set at 1943' | Perforations | To |
| Type Completion (Describe) Gas, single zone | | Type Fluid Production SW | | Pump Unit or Traveling Plunger? Yes / No No | |
| Producing Thru (Annulus / Tubing) Tubing | | % Carbon Dioxide 0 | | % Nitrogen 31 | |
| Vertical Depth(H) | | Pressure Taps | | (Meter Run) (Prover) Size | |

Pressure Buildup: Shut in 6/7 20 11 at 10 AM (AM) (PM) Taken 6/9 20 11 at 10 AM (AM) (PM)
Well on Line: Started 20 at (AM) (PM) Taken 20 at (AM) (PM)

OBSERVED SURFACE DATA

Duration of Shut-in _____ Hours

| Static / Dynamic Property | Orifice Size (inches) | Circle one: Meter or Prover Pressure psig (Pm) | Pressure Differential in Inches H ₂ O | Flowing Temperature t | Well Head Temperature t | Casing Wellhead Pressure (P _w) or (P _i) or (P _c) | | Tubing Wellhead Pressure (P _w) or (P _i) or (P _c) | | Duration (Hours) | Liquid Produced (Barrels) |
|---------------------------|-----------------------|--|--|-----------------------|-------------------------|--|------|--|------|------------------|---------------------------|
| | | | | | | psig | psia | psig | psia | | |
| Shut-in | | | | | | 105# | | | | | |
| Flow | | | | | | | | | | | |

FLOW STREAM ATTRIBUTES

| Plate Coefficient (F _s) (F _v) Mcfd | Circle one: Meter or Prover Pressure psia | Press Extension $\sqrt{P_m \times h}$ | Gravity Factor F _g | Flowing Temperature Factor F _t | Deviation Factor F _{pv} | Metered Flow R (Mcf/d) | GOR (Cubic Feet/ Barrel) | Flowing Fluid Gravity G _m |
|--|---|---------------------------------------|-------------------------------|---|----------------------------------|------------------------|--------------------------|--------------------------------------|
| | | | | | | | | |

(OPEN FLOW) (DELIVERABILITY) CALCULATIONS

(P_o)² = _____ : (P_w)² = _____ : P_d = _____ % (P_c - 14.4) + 14.4 = _____ : (P_w)² = 0.207
(P_o)² = _____

| (P _c) ² - (P _a) ² or (P _c) ² - (P _d) ² | (P _c) ² - (P _w) ² | Choose formula 1 or 2: 1. P _c ² - P _a ² 2. P _c ² - P _d ² divided by: P _c ² - P _w ² | LOG of formula 1. or 2. and divide by: $\left[\frac{P_c^2 - P_w^2}{P_c^2 - P_a^2} \right]$ | Backpressure Curve Slope = "n" or Assigned Standard Slope | n x LOG $\left[\frac{P_c^2 - P_w^2}{P_c^2 - P_a^2} \right]$ | Antilog | Open Flow Deliverability Equals R x Antilog (Mcf/d) |
|--|---|---|---|---|--|---------|---|
| | | | | | | | |

Open Flow Mcfd @ 14.65 psia Deliverability Mcfd @ 14.65 psia

The undersigned authority, on behalf of the Company, states that he is duly authorized to make the above report and that he has knowledge of the facts stated therein, and that said report is true and correct. Executed this the _____ day of _____, 20 _____.

Witness (if any)

For Commission

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For Company

Checked by

I declare under penalty of perjury under the laws of the state of Kansas that I am authorized to request exempt status under Rule K.A.R. 82-3-304 on behalf of the operator Becker Oil Corporation and that the foregoing pressure information and statements contained on this application form are true and correct to the best of my knowledge and belief based upon available production summaries and lease records of equipment installation and/or upon type of completion or upon use being made of the gas well herein named.

I hereby request a one-year exemption from open flow testing for the McCune #1A gas well on the grounds that said well:

(Check one)

- is a coalbed methane producer
- is cycled on plunger lift due to water
- is a source of natural gas for injection into an oil reservoir undergoing ER
- is on vacuum at the present time; KCC approval Docket No. _____
- is not capable of producing at a daily rate in excess of 250 mcf/D

I further agree to supply to the best of my ability any and all supporting documents deemed by Commission staff as necessary to corroborate this claim for exemption from testing.

Date: 6/10/11

Signature: *Clyde M Becker*
Title: President

Instructions: If a gas well meets one of the eligibility criteria set out in KCC regulation K.A.R. 82-3-304, the operator may complete the statement provided above in order to claim exempt status for the gas well.

At some point during the current calendar year, wellhead shut-in pressure shall have been measured after a minimum of 24 hours shut-in/buildup time and shall be reported on the front side of this form under **OBSERVED SURFACE DATA**. Shut-in pressure shall thereafter be reported yearly in the same manner for so long as the gas well continues to meet the eligibility criterion or until the claim of eligibility for exemption **IS** denied.

The G-2 form conveying the newest shut-in pressure reading shall be filed with the Wichita office no later than December 31 of the year for which it's intended to acquire exempt status for the subject well. The form must be signed and dated on the front side as though it was a verified report of annual test results.

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GAS VOLUME STATEMENT

BECKER OIL CORPORATION
Measured Conditions

999 -- MCLUNE A-1
April, 2011

| | | | | | | | | | | | | | |
|------------------------------|----------|----------------------------|--------------|---------------------------|----------------|-------------------|-------------|--------------------|-------|-------|-------|-------|-------|
| Pressure Base: 14.730 psia | | Temperature Base: 50.00 °F | | HV Cond: Wet | | Meter Type: Chart | | Contract Hr.: 9 AM | | | | | |
| Water Vapor Corr. Technique: | | | | Water Vapor Corr. Method: | | | | | | | | | |
| CO2 | N2 | H2O | H2S | O2 | He | C1 | C2 | C3 | I-C4 | N-C4 | I-C5 | N-C5 | C6+ |
| 0.030 | 31.010 | | 0.0000 | 0.000 | 0.810 | 65.080 | 1.930 | 0.900 | 0.100 | 0.110 | 0.010 | 0.000 | 0.000 |
| Tube I.D. | Rotation | Meter Range | Tap Location | Tap Type | Atmos Pressure | Calc. Method | Spv Method | | | | | | |
| 3.058 in | 8 Days | 500# 100" 0 - 100°F | Downstream | Flange | 13.200 psi | AGA3-1992 | AGA8-Detail | | | | | | |

| Day | Differential Pressure (in. H2O) | Pressure (PSIA) | Temperature (°F) | Hours Flow | Relative Density | Plate (inches) | Volume (Mcf) | Heating Value (BTU/scf) | Energy (MMBTU) |
|-------|---------------------------------|-----------------|------------------|------------|------------------|----------------|--------------|-------------------------|----------------|
| 1 | 3.51 | 47.23 | 60.00 | 24.00 | 0.7017 | | | | |
| 2 | 3.31 | 48.00 | 60.00 | 24.00 | 0.7017 | 0.750 | 42 | 712.00 | 30 |
| 3 | 3.71 | 48.19 | 60.00 | 24.00 | 0.7017 | 0.750 | 41 | 712.00 | 29 |
| 4 | 3.94 | 47.80 | 60.00 | 24.00 | 0.7017 | 0.750 | 44 | 712.00 | 29 |
| 5 | 3.77 | 50.17 | 60.00 | 24.00 | 0.7017 | 0.750 | 45 | 712.00 | 31 |
| 6 | 3.52 | 50.11 | 60.00 | 24.00 | 0.7017 | 0.750 | 45 | 712.00 | 32 |
| 7 | 3.60 | 45.84 | 60.00 | 24.00 | 0.7017 | 0.750 | 44 | 712.00 | 32 |
| 8 | 3.29 | 48.84 | 60.00 | 24.00 | 0.7017 | 0.750 | 42 | 712.00 | 31 |
| 9 | 3.21 | 46.48 | 60.00 | 24.00 | 0.7017 | 0.750 | 40 | 712.00 | 30 |
| 10 | 3.44 | 47.62 | 60.00 | 24.00 | 0.7017 | 0.750 | 40 | 712.00 | 28 |
| 11 | 3.58 | 48.21 | 60.00 | 24.00 | 0.7017 | 0.750 | 42 | 712.00 | 29 |
| 12 | 3.68 | 49.27 | 60.00 | 24.00 | 0.7017 | 0.750 | 43 | 712.00 | 30 |
| 13 | 2.16 | 52.03 | 60.00 | 24.00 | 0.7017 | 0.750 | 24 | 712.00 | 31 |
| 14 | 2.38 | 49.36 | 60.00 | 19.34 | 0.7017 | 0.750 | 31 | 712.00 | 31 |
| 15 | 4.57 | 45.77 | 60.00 | 24.00 | 0.7017 | 0.750 | 26 | 712.00 | 22 |
| 16 | 3.03 | 46.30 | 60.00 | 24.00 | 0.7017 | 0.750 | 46 | 712.00 | 19 |
| 17 | 3.71 | 49.21 | 60.00 | 24.00 | 0.7017 | 0.750 | 44 | 712.00 | 33 |
| 18 | 3.63 | 50.80 | 60.00 | 24.00 | 0.7017 | 0.750 | 44 | 712.00 | 31 |
| 19 | 3.98 | 48.70 | 60.00 | 24.00 | 0.7017 | 0.750 | 44 | 712.00 | 32 |
| 20 | 4.09 | 46.60 | 60.00 | 24.00 | 0.7017 | 0.750 | 45 | 712.00 | 32 |
| 21 | 3.87 | 49.27 | 60.00 | 24.00 | 0.7017 | 0.750 | 45 | 712.00 | 32 |
| 22 | 3.55 | 47.76 | 60.00 | 24.00 | 0.7017 | 0.750 | 45 | 712.00 | 32 |
| 23 | 3.84 | 53.34 | 60.00 | 24.00 | 0.7017 | 0.750 | 45 | 712.00 | 32 |
| 24 | 3.73 | 52.66 | 60.00 | 24.00 | 0.7017 | 0.750 | 43 | 712.00 | 30 |
| 25 | 3.03 | 50.31 | 60.00 | 24.00 | 0.7017 | 0.750 | 47 | 712.00 | 30 |
| 26 | 3.83 | 50.02 | 60.00 | 24.00 | 0.7017 | 0.750 | 46 | 712.00 | 33 |
| 27 | 3.94 | 49.76 | 60.00 | 24.00 | 0.7017 | 0.750 | 46 | 712.00 | 33 |
| 28 | 3.38 | 49.40 | 60.00 | 24.00 | 0.7017 | 0.750 | 45 | 712.00 | 33 |
| 29 | 3.15 | 49.41 | 60.00 | 24.00 | 0.7017 | 0.750 | 46 | 712.00 | 32 |
| 30 | 3.58 | 47.04 | 60.00 | 24.00 | 0.7017 | 0.750 | 42 | 712.00 | 33 |
| TOTAL | 3.63 | 48.68 | 60.00 | 15.34 | 0.7017 | 0.50 | 43 | 712.00 | 29 |
| | | | | | | | 1.281 | | 912 |

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12/27/2010 16:44.06

Meter No: 4471696A
 Meter Name: MCCUNE
 Operator Number: 743361
 Operator Name: BECKER OIL CORPORATION
 Contract Number: 431180 CCT Number 43118001
 Contracted Party: BECKER OIL CORPORATION



**ONEOK
 FIELD
 SERVICES**

Business Date: November 2010

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Production Month: November 2010
 System Name: CHENEY GAS SYSTEM
 Pressure Base: 14.65
 BTU Basis: DRY
 Alloc. Decimal: 1.0000000
 Tax Exempt Dec: 0.000000

AP

System Totals

LIQUIDS

| | Theoretical Gal/LT | Actual Gal/LT |
|----------------|--------------------|---------------|
| ETHANE | 2,318,601.33 | 1,675,854.00 |
| PROPANE | 1,191,351.89 | 995,850.00 |
| ISO BUTANE | 192,011.77 | 165,737.00 |
| NORMAL BUTANE | 467,933.23 | 396,643.00 |
| ISO PENTANE | 143,109.49 | 109,896.00 |
| NORMAL PENTANE | 176,911.13 | 130,160.00 |
| HEXANES | 367,788.86 | 193,434.00 |

TOTAL 3,667,574.00

**WELLHEAD/
 RESIDUE**

| | MCF | MMBTU |
|---------------------|--------------|--------------|
| GROSS WELLHEAD | 1,590,009.76 | 1,795,022.69 |
| NET DELV WELLHEAD | 1,590,010.63 | 1,795,023.67 |
| SHRINKAGE | 128,213.91 | 309,298.35 |
| THEORETICAL RESIDUE | 1,461,796.72 | 1,485,725.32 |
| RESIDUE PRODUCED | 0.00 | 0.00 |
| RESIDUE RETURNED | 0.00 | 0.00 |
| RES AVAIL FOR SALE | 1,302,871.81 | 1,263,486.00 |
| RESIDUE SOLD | 1,302,871.81 | 1,263,486.00 |

Meter Totals

| Theoretical Gal/LT | Actual Gal/LT | In Kind Gal/LT | Producer Percent | Producer Gallons | Price | Value |
|--------------------|---------------|----------------|------------------|------------------|-----------|----------|
| 819.03 | 591.98 | | 85.00 | 503.18 | \$0.43789 | \$220.34 |
| 271.36 | 226.82 | | 85.00 | 192.80 | \$1.13311 | \$218.46 |
| 24.80 | 21.40 | | 85.00 | 18.19 | \$1.50241 | \$27.33 |
| 39.68 | 33.64 | | 85.00 | 28.59 | \$1.48150 | \$42.35 |
| 17.71 | 9.32 | | 85.00 | 7.92 | \$1.81904 | \$14.41 |
| | 883.16 | 0.00 | | 750.68 | | \$522.89 |

| Actual | | In Kind | | Producer | | Price | Value |
|----------|----------|---------|-------|----------|--------|--------|---------------------|
| MCF | MMBTU | MCF | MMBTU | Percent | MCF | MMBTU | |
| 1,417.00 | 1,186.82 | | | | | | |
| 1,417.00 | 1,186.82 | | | | | | |
| 32.48 | 66.76 | | | | | | |
| 1,384.52 | 1,120.06 | | | | | | |
| 982.21 | 952.52 | | | | | | |
| 0.00 | 0.00 | | | | | | |
| 982.21 | 952.52 | | | | | | |
| 982.21 | 952.52 | 0.00 | 0.00 | 85.00 | 834.88 | 809.64 | \$3.0100 \$2,437.02 |

TAX DETAIL

| TAX TYPE | TAX AMT |
|------------------------------|---------|
| KCC - KANSAS CORPORATION TAX | 18.28 |
| KST - KANSAS SEVERANCE TAX | 125.59 |

FEES/ADJUSTMENTS

| Fee Type | Fee Volume | Fee Rate | Value | Comments |
|-------------|------------|----------|---------|----------|
| COMPRESSION | 1,186.82 | \$0.0500 | \$59.34 | |

\$59.34

| Comments |
|--------------------------------|
| KSWI 1.21 REVISED 9/28/2010 |

| ONEOK Contact Information | |
|---------------------------|---|
| Primary: | LARRY DEASON 918-732-1416 LDEASON@ONEOK.COM |
| Measurement: | ONEOK ENERGY MEASUREMENT GROUP 918-732-1400 OFS_MEASUREMENT@ONEOK.COM |
| Contract: | JOICE HIGHFILL 918-591-5152 |

| Gas Analysis | |
|----------------|---------|
| GPM | Mol % |
| Helium | 0.6859 |
| Nitrogen | 19.3631 |
| Carbon Dioxide | 0.0154 |
| Sulfur | 0.0000 |
| Methane | 76.8902 |
| Ethane | 0.5780 |
| Propane | 0.1915 |
| Iso-Butane | 0.0175 |
| Normal Butane | 0.0280 |
| Iso-Pentane | 0.0000 |
| Normal Pentane | 0.0000 |
| Hexanes Plus | 0.0125 |
| Other | 0.0000 |
| 0.8275 | 99.9999 |

| Summary | Value |
|-------------------------|------------|
| Residue | \$2,437.02 |
| Liquids | \$522.89 |
| Helium | \$0.00 |
| Fees/ADJ's | (\$59.34) |
| Subtotal (Before Taxes) | \$2,900.57 |
| Taxes | (\$143.87) |
| Net Due | \$2,756.70 |