

# Kansas Corporation Commission One Point Stabilized Open Flow or Deliverability Test

Form G 2  
(Rev. 7/03)

Type Test:

- Open Flow  
 Deliverability

Test Date: **11/21/2012**

API No. **15081219890000**

Company <b>OXY USA Inc</b>		Lease <b>PHOENIX A 1</b>		Well Number	
County <b>Haskell</b>	Location <b>330' FNL &amp; 620' FEL</b>	Section <b>23</b>	TWP <b>30S</b>	RNG (E/W) <b>33W</b>	Acres Attributed <b>640</b>
Field <b>TICE</b>		Reservoir <b>Chester</b>	Gas Gathering Connection <b>Frontstreet</b>		
Completion Date <b>10/25/2012</b>		Plug Back Total Depth <b>5,669'</b>		Packer Set at	
Casing Size <b>5 1/2"</b>	Weight <b>17.0#</b>	Internal Diameter <b>4.892"</b>	Set at <b>5,710'</b>	Perforations <b>5,403'</b>	To <b>5,430'</b>
Tubing Size	Weight	Internal Diameter	Set at	Perforations	To

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Type Completion (Describe) <b>SINGLE-GAS</b>	Type Fluid Production <b>WATER</b>	Pump Unit or Traveling Plunger? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	
Producing Thru (Annulus / Tubing) <b>Annulus</b>	% Carbon Dioxide <b>0.330%</b>	% Nitrogen <b>10.198%</b>	Gas Gravity Gg <b>0.788</b>
Vertical Depth (H) <b>5,417'</b>	Pressure Taps <b>Flange</b>	(Meter Run) (Prover) Size <b>3.068"</b>	
Pressure Buildup: Shut in <u>11/17</u> 20 <u>12</u> at <u>9:00</u> <input checked="" type="checkbox"/> AM <input type="checkbox"/> PM Taken <u>11/20</u> 20 <u>12</u> at <u>9:00</u> <input checked="" type="checkbox"/> AM <input type="checkbox"/> PM			
Well on Line: Started <u>11/20</u> 20 <u>12</u> at <u>9:00</u> <input checked="" type="checkbox"/> AM <input type="checkbox"/> PM Taken <u>11/21</u> 20 <u>12</u> at <u>9:00</u> <input checked="" type="checkbox"/> AM <input type="checkbox"/> PM			

**OBSERVED SURFACE DATA**

Duration of Shut in 72 Hours

Static / Dynamic Property	Orifice Size (inches)	Circle one: Meter or Prover Pressure psig (Pm)	Pressure Differential in Inches H <sub>2</sub> O	Flowing Temperature t	Well Head Temperature t	Casing Wellhead Pressure (P <sub>w</sub> ) or (P <sub>i</sub> ) or (P <sub>c</sub> )		Tubing Wellhead Pressure (P <sub>w</sub> ) or (P <sub>i</sub> ) or (P <sub>c</sub> )		Duration (Hours)	Liquid Produced (Barrels)
						psig	psia	psig	psia		
Shut In						<b>758.0</b>	<b>772.4</b>		<b>0</b>		<b>0</b>
Flow	<b>2.000</b>	<b>12.4</b>	<b>5</b>	<b>65</b>	<b>75</b>	<b>439.5</b>	<b>453.9</b>		<b>0.0</b>	<b>24</b>	<b>0</b>

**FLOW STREAM ATTRIBUTES**

Plate Coefficient (F <sub>d</sub> ) (F <sub>p</sub> ) Mcfd	Circle one: Meter or Prover Pressure psia	Press Extension $\sqrt{P_m \times h}$	Gravity Factor F <sub>g</sub>	Flowing Temperature Factor F <sub>T</sub>	Deviation Factor F <sub>w</sub>	Metered Flow R (Mcfd)	GOR (Cubic Feet/Barrel)	Flowing Fluid Gravity G <sub>m</sub>
<b>21.8600</b>	<b>26.8</b>	<b>11.58</b>	<b>1.1265</b>	<b>0.9952</b>	<b>1.0029</b>	<b>285</b>	<b>None</b>	<b>0.717</b>

**(OPEN FLOW) (DELIVERABILITY) CALCULATIONS**

(P<sub>c</sub>)<sup>2</sup> = **596.6** ; (P<sub>w</sub>)<sup>2</sup> = **206.0** ; P<sub>d</sub> = \_\_\_\_\_ % (P<sub>c</sub> 14.4) + 14.4 = \_\_\_\_\_ ; (P<sub>a</sub>)<sup>2</sup> = **0.207**  
(P<sub>d</sub>)<sup>2</sup> = **0**

(P <sub>c</sub> ) <sup>2</sup> (P <sub>a</sub> ) <sup>2</sup> or (P <sub>c</sub> ) <sup>2</sup> (P <sub>d</sub> ) <sup>2</sup>	(P <sub>c</sub> ) <sup>2</sup> (P <sub>w</sub> ) <sup>2</sup>	Choose Formula 1 or 2: 1. P <sub>c</sub> <sup>2</sup> P <sub>a</sub> <sup>2</sup> 2. P <sub>c</sub> <sup>2</sup> P <sub>d</sub> <sup>2</sup> divided by: P <sub>c</sub> <sup>2</sup> P <sub>w</sub> <sup>2</sup>	LOG of formula 1. or 2. and divide by:	Backpressure Curve Slope = "n" or Assigned Standard Slope	n x LOG	Antilog	Open Flow Deliverability Equals R x Antilog (Mcfd)
<b>596.4</b>	<b>390.6</b>	<b>1.5269</b>	<b>0.1838</b>	<b>0.8005</b>	<b>0.1471</b>	<b>1.4031</b>	<b>400</b>

Open Flow **400** Mcfd @ 14.65 psia      Deliverability Mcfd @ 14.65 psia

The undersigned authority, on behalf of the Company, states that he is duly authorized to make the above report and that he has knowledge of the facts stated therein, and that said report is true and correct. Executed this the 26 day of November, 2012

\_\_\_\_\_  
Witness  
\_\_\_\_\_  
For Commission

**OXY USA INC**  
For Company  
**David Ogden - OXY USA Inc.**  
Checked by \_\_\_\_\_

**State of Kansas - Corporation Commission  
Multipoint Back Pressure Test**

Form CG-1  
(Rev. 10/96)

Type Test:  Initial  Annual  Special

Test Date: **11/21/2012**

Company: **OXY USA Inc** Lease: **PHOENIX A 1** Well Number: \_\_\_\_\_

County: **Haskell** Location: **330' FNL & 620' FEL** Section: **23** TWP: **30S** RNG (E/W): **33W** Acres Attributed: **640**

API No: **15081219890000** Reservoir: **Chester** Pipeline Connection: **Frontstreet**

Completion Date: **10/25/2012** Plug Back Total Depth: **5,669'** Packer Set at: \_\_\_\_\_

Casing Size: **5 1/2"** Weight: **17.0#** Internal Diameter: **4.892"** Set at: **5,710'** Perforations: **5,403'** To: **5,430'**

Tubing Size: \_\_\_\_\_ Weight: \_\_\_\_\_ Internal Diameter: \_\_\_\_\_ Set at: \_\_\_\_\_ Perforations: \_\_\_\_\_ To: \_\_\_\_\_

Type Completion (Describe): **SINGLE-GAS** Type Fluid Production: **WATER**

Producing Thru (Annulus / Tubing): **Annulus** Reservoir Temperature °F: **133** BAR PRESS -P<sub>a</sub>: **14.4 Psia**

Gas Gravity - G<sub>g</sub>: **0.788** % Carbon Dioxide: **0.330%** % Nitrogen: **10.198%**

Vertical Depth (H): **5,417'** Type Meter Connection: **Flange** (Meter Run) (Prover) Size: **3.068"**

**OBSERVED DATA**

Duration of Shut-in **72** Hours

Rate No	Orifice Size (inches)	Circle One: Meter Prover Pressure psig (P <sub>m</sub> )	Pressure Differential in inches H <sub>2</sub> O	Flowing Temperature t	Well Head Temperature t	Casing Wellhead Pressure (P <sub>w</sub> ) or (P <sub>i</sub> ) or (P <sub>e</sub> )		Tubing Wellhead Pressure (P <sub>w</sub> ) or (P <sub>i</sub> ) or (P <sub>e</sub> )		Duration (Hours)	Liquid Produced (Barrels)
						psig	psia	psig	psia		
<b>Shut-In</b>					<b>75</b>	<b>758.0</b>	<b>772.4</b>	<b>0.0</b>	<b>0.0</b>	<b>72</b>	
<b>1</b>	<b>2.000</b>	<b>11.4</b>	<b>1.1</b>	<b>66</b>	<b>75</b>	<b>731.0</b>	<b>745.4</b>	<b>0.0</b>	<b>0.0</b>	<b>1</b>	<b>0</b>
<b>2</b>	<b>2.000</b>	<b>12.1</b>	<b>3.8</b>	<b>70</b>	<b>75</b>	<b>698.8</b>	<b>713.2</b>	<b>0.0</b>	<b>0.0</b>	<b>1</b>	<b>0</b>
<b>3</b>	<b>2.000</b>	<b>13.6</b>	<b>10.2</b>	<b>75</b>	<b>75</b>	<b>640.5</b>	<b>654.9</b>	<b>0.0</b>	<b>0.0</b>	<b>1</b>	<b>0</b>
<b>4</b>	<b>2.000</b>	<b>15.6</b>	<b>20.6</b>	<b>75</b>	<b>75</b>	<b>549.3</b>	<b>563.7</b>	<b>0.0</b>	<b>0.0</b>	<b>1</b>	<b>0</b>
<b>5</b>											

**RATE OF FLOW CALCULATIONS**

Rate No	Plate Coefficient (F <sub>s</sub> ) (F <sub>p</sub> ) Mcfd	Circle One: Meter Prover Pressure psia	Press Extension $\sqrt{P_m \times h}$	Gravity Factor F <sub>g</sub>	Flowing Temperature Factor F <sub>t</sub>	Deviation Factor F <sub>d</sub>	Rate of Flow Q Mcfd	GOR (Cubic Feet/Barrel)	Flowing Fluid Gravity G <sub>m</sub>
<b>1</b>	<b>21.86</b>	<b>25.8</b>	<b>5.33</b>	<b>1.1265</b>	<b>0.9943</b>	<b>1.003</b>	<b>131</b>		<b>0.788</b>
<b>2</b>	<b>21.86</b>	<b>26.5</b>	<b>10.03</b>	<b>1.1265</b>	<b>0.9905</b>	<b>1.003</b>	<b>245</b>		<b>0.788</b>
<b>3</b>	<b>21.86</b>	<b>28.0</b>	<b>16.90</b>	<b>1.1265</b>	<b>0.9859</b>	<b>1.003</b>	<b>411</b>		<b>0.788</b>
<b>4</b>	<b>21.86</b>	<b>30.0</b>	<b>24.86</b>	<b>1.1265</b>	<b>0.9859</b>	<b>1.003</b>	<b>605</b>		<b>0.788</b>
<b>5</b>									

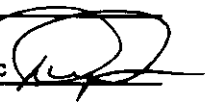
**PRESSURE CALCULATIONS**

Rate No	P <sub>i</sub> Psia	P <sub>e</sub> Psia	P <sub>w</sub> Psia	(P <sub>e</sub> ) <sup>2</sup> Thousands	(P <sub>w</sub> ) <sup>2</sup> Thousands	Plotting Points		% Shut-In (P <sub>w</sub> - P <sub>a</sub> ) (P <sub>e</sub> - P <sub>a</sub> )
						(P <sub>e</sub> ) <sup>2</sup> - (P <sub>w</sub> ) <sup>2</sup> Thousands	Q Mcfd	
<b>1</b>		<b>772.4</b>	<b>745.4</b>	<b>596.6</b>	<b>555.6</b>	<b>41.0</b>	<b>131</b>	<b>96.4%</b>
<b>2</b>		<b>772.4</b>	<b>713.2</b>	<b>596.6</b>	<b>508.7</b>	<b>87.9</b>	<b>245</b>	<b>92.2%</b>
<b>3</b>		<b>772.4</b>	<b>654.9</b>	<b>596.6</b>	<b>428.9</b>	<b>167.7</b>	<b>411</b>	<b>84.5%</b>
<b>4</b>		<b>772.4</b>	<b>563.7</b>	<b>596.6</b>	<b>317.8</b>	<b>278.8</b>	<b>605</b>	<b>72.5%</b>
<b>5</b>								

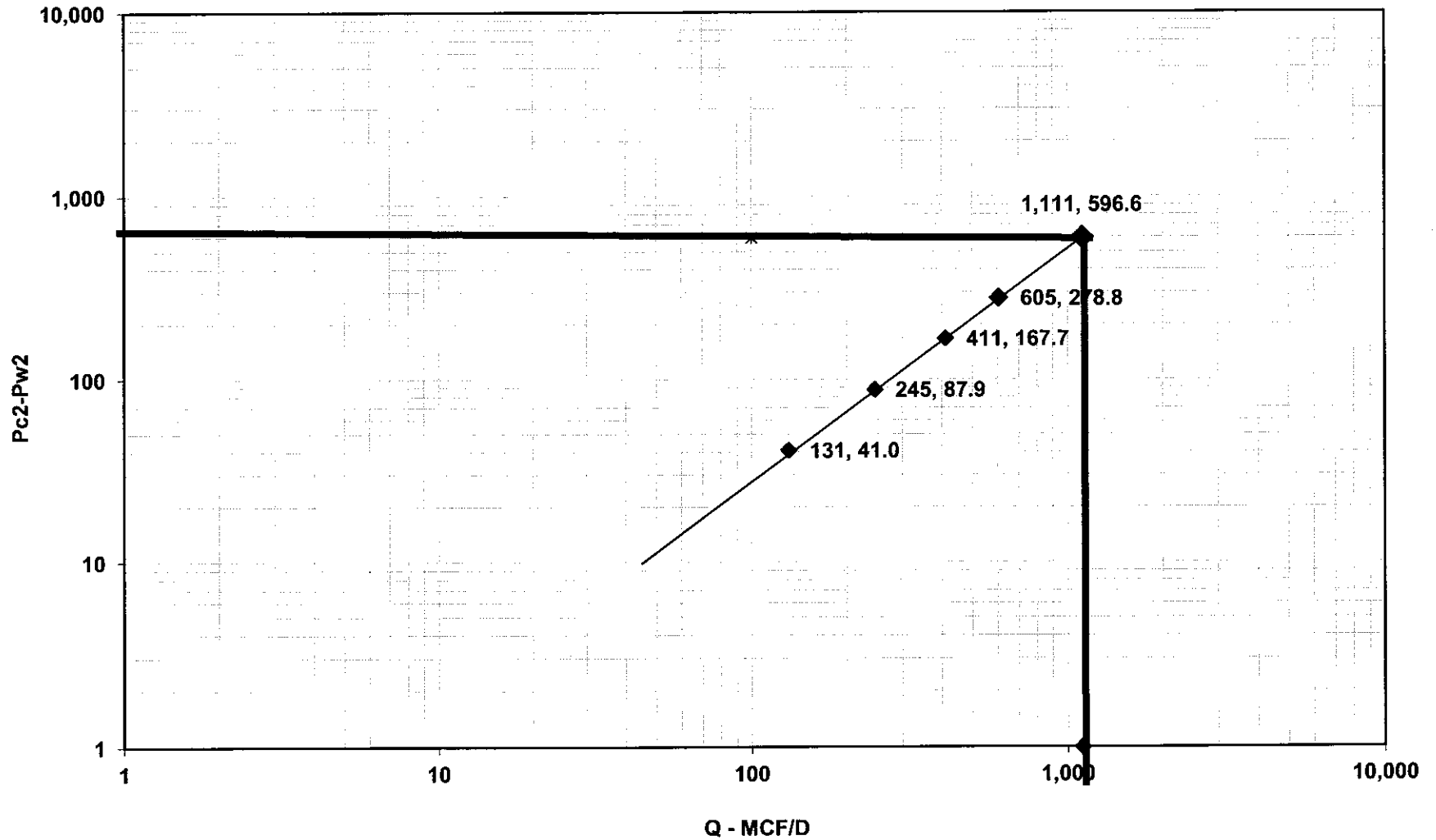
Indicated Wellhead Open Flow **1,111** Mcfd @ 14.65 psia "n" = **0.799**

The undersigned authority, on behalf of the Company, states that he is duly authorized to make the above report and that he has knowledge of the facts stated therein, and that said report is true and correct. Executed this the **25** day of **November** **2012**

\_\_\_\_\_  
Witness (If any)  
\_\_\_\_\_  
For Commission

**OXY USA INC.**  
For Company  
**David Ogden - OXY USA Inc**  
Checked by 

# PHOENIX A 1 Section 23, T30S, R33W Haskell County, Kansas



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