

# KANSAS CORPORATION COMMISSION ONE POINT STABILIZED OPEN FLOW OR DELIVERABILITY TEST

Type Test:

(See Instructions on Reverse Side)

15-077-21447-00-01

- Open Flow  
 Deliverability

Test Date:  
11-27-12

Company <b>Union Valley Petroleum Corporation</b>			Lease <b>Witters</b>		Well Number <b>1-28</b>
County <b>HARPER</b>	Location <b>C W/2 NW</b>	Section <b>28</b>	TWP <b>33S</b>	RNG (E/W) <b>6W</b>	Acres Attributed <b>80</b>
Field <b>Anthony</b>		Reservoir <b>Mississippi</b>	Gas Gathering Connection <b>Atlas</b>		
Completion Date <b>3-13-03</b>		Plug Back Total Depth <b>4880</b>	Packer Set at <b>none</b>		
Casing Size <b>5.5</b>	Weight <b>15.5</b>	Internal Diameter <b>4.96</b>	Set at <b>4920</b>	Perforations <b>4464</b>	To <b>4474</b>
Tubing Size <b>2.375</b>	Weight <b>4.7</b>	Internal Diameter <b>1.995</b>	Set at <b>4553</b>	Perforations	To
Type Completion (Describe) <b>single</b>		Type Fluid Production <b>water/oil</b>	Pump Unit or Traveling Plunger? Yes / No <b>pumping unit</b>		
Producing Thru (Annulus / Tubing) <b>annulus</b>		% Carbon Dioxide <b>.1673</b>	% Nitrogen <b>5.519</b>	Gas Gravity - G <sub>g</sub> <b>.6915</b>	
Vertical Depth(H)		Pressure Taps		(Meter Run) (Prover) Size	
Pressure Buildup: Shut in <b>11-27</b> 20 <b>12</b> at <b>900 am</b> (AM) (PM) Taken <b>11-28</b> 20 <b>12</b> at <b>900</b> (AM) (PM)					
Well on Line: Started _____ 20 _____ at _____ (AM) (PM) Taken _____ 20 _____ at _____ (AM) (PM)					

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### OBSERVED SURFACE DATA

Duration of Shut-in \_\_\_\_\_ Hours

Static / Dynamic Property	Orifice Size (inches)	Circle one: Meter or Prover Pressure psig (P <sub>m</sub> )	Pressure Differential in Inches H <sub>2</sub> O	Flowing Temperature t	Well Head Temperature t	Casing Wellhead Pressure (P <sub>w</sub> ) or (P <sub>i</sub> ) or (P <sub>c</sub> )		Tubing Wellhead Pressure (P <sub>w</sub> ) or (P <sub>i</sub> ) or (P <sub>c</sub> )		Duration (Hours)	Liquid Produced (Barrels)
						psig	psia	psig	psia		
Shut-In							<b>341</b>				
Flow											

### FLOW STREAM ATTRIBUTES

Plate Coefficient (F <sub>c</sub> ) (F <sub>p</sub> ) Mcfd	Circle one: Meter or Prover Pressure psia	Press Extension $\sqrt{P_m \times h}$	Gravity Factor F <sub>g</sub>	Flowing Temperature Factor F <sub>t</sub>	Deviation Factor F <sub>pv</sub>	Metered Flow R (Mcfd)	GOR (Cubic Feet/ Barrel)	Flowing Fluid Gravity G <sub>m</sub>

### (OPEN FLOW) (DELIVERABILITY) CALCULATIONS

(P<sub>a</sub>)<sup>2</sup> = 0.207

(P<sub>c</sub>)<sup>2</sup> = \_\_\_\_\_ : (P<sub>w</sub>)<sup>2</sup> = \_\_\_\_\_ : P<sub>d</sub> = \_\_\_\_\_ % (P<sub>c</sub> - 14.4) + 14.4 = \_\_\_\_\_ : (P<sub>d</sub>)<sup>2</sup> = \_\_\_\_\_

(P <sub>c</sub> ) <sup>2</sup> - (P <sub>a</sub> ) <sup>2</sup> or (P <sub>c</sub> ) <sup>2</sup> - (P <sub>d</sub> ) <sup>2</sup>	(P <sub>c</sub> ) <sup>2</sup> - (P <sub>w</sub> ) <sup>2</sup>	Choose formula 1 or 2: 1. P <sub>c</sub> <sup>2</sup> - P <sub>a</sub> <sup>2</sup> 2. P <sub>c</sub> <sup>2</sup> - P <sub>d</sub> <sup>2</sup> divided by: P <sub>c</sub> <sup>2</sup> - P <sub>w</sub> <sup>2</sup>	LOG of formula 1. or 2. and divide by: $\frac{P_c^2 - P_a^2}{P_c^2 - P_w^2}$	Backpressure Curve Slope = "n" or Assigned Standard Slope	n x LOG $\left[ \frac{P_c^2 - P_a^2}{P_c^2 - P_w^2} \right]$	Antilog	Open Flow Deliverability Equals R x Antilog (Mcfd)

Open Flow \_\_\_\_\_ Mcfd @ 14.65 psia      Deliverability \_\_\_\_\_ Mcfd @ 14.65 psia

The undersigned authority, on behalf of the Company, states that he is duly authorized to make the above report and that he has knowledge of the facts stated therein, and that said report is true and correct. Executed this the 12 day of December, 20 12.

\_\_\_\_\_  
Witness (if any)      For Company

\_\_\_\_\_  
For Commission      Checked by

I declare under penalty of perjury under the laws of the state of Kansas that I am authorized to request exempt status under Rule K.A.R. 82-3-304 on behalf of the operator Union Valley Petroleum Corporation and that the foregoing pressure information and statements contained on this application form are true and correct to the best of my knowledge and belief based upon available production summaries and lease records of equipment installation and/or upon type of completion or upon use being made of the gas well herein named.

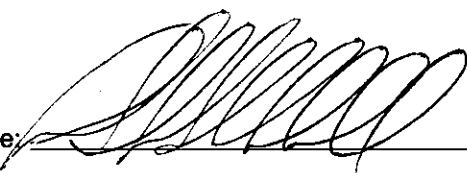
I hereby request a one-year exemption from open flow testing for the Witters #1-28 gas well on the grounds that said well:

(Check one)

- is a coalbed methane producer
- is cycled on plunger lift due to water
- is a source of natural gas for injection into an oil reservoir undergoing ER
- is on vacuum at the present time; KCC approval Docket No. \_\_\_\_\_
- is not capable of producing at a daily rate in excess of 250 mcf/D

I further agree to supply to the best of my ability any and all supporting documents deemed by Commission staff as necessary to corroborate this claim for exemption from testing.

Date: 12-12-12

Signature:  \_\_\_\_\_  
Title: President

**Instructions:** If a gas well meets one of the eligibility criteria set out in KCC regulation K.A.R. 82-3-304, the operator may complete the statement provided above in order to claim exempt status for the gas well.

At some point during the current calendar year, wellhead shut-in pressure shall have been measured after a minimum of 24 hours shut-in/buildup time and shall be reported on the front side of this form under **OBSERVED SURFACE DATA**. Shut-in pressure shall thereafter be reported yearly in the same manner for so long as the gas well continues to meet the eligibility criterion or until the claim of eligibility for exemption **IS** denied.

The G-2 form conveying the newest shut-in pressure reading shall be filed with the Wichita office no later than December 31 of the year for which it's intended to acquire exempt status for the subject well. The form must be signed and dated on the front side as though it was a verified report of annual test results.

95401046 *Wichita #1 - 28*  
 Analysis

Date-Time: 09/21/12 09:43 Analysis Time: 230 Cycle Time: 240  
 Stream: 1 Stream 1 Mode: ANLY Cycle Start Time: 09:39  
 Analyzer: 204295 Strm Seq:1  
 95401046 H2S 0.0  
 PSIG 30.3 TEMP 71.3

Component Name	Mole Percent	Gallons/1000 SCF	BTU Gross	Relative Density
C6+ 47/35/17	0.6582	0.2937	34.81	0.0218
PROPANE	3.0601	0.8428	77.17	0.0466
i-BUTANE	0.4090	0.1338	13.33	0.0082
n-BUTANE	1.0626	0.3349	34.75	0.0213
i-PENTANE	0.2436	0.0891	9.77	0.0061
n-PENTANE	0.3348	0.1213	13.45	0.0083
NITROGEN	5.5190	0.0000	0.00	0.0534
METHANE	81.7748	0.0000	827.84	0.4530
CARBON DIOXIDE	0.1673	0.0000	0.00	0.0025
ETHANE	6.7706	1.8102	120.10	0.0703
TOTALS	100.0000	3.6259	1131.22	0.6915

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'\*' indicates user-defined components

Compressibility Factor (1/Z) @ 14.73000 PSIA & 60.0 DEG.F= 1.00289

Base Pressures	14.73000	
Gross Dry BTU	= 1134.48	Corrected/Z
Gross SAT BTU	= 1114.74	Corrected/Z
Gallons/1000 SCF C2+	= 3.6259	
Gallons/1000 SCF C3+	= 1.8157	
Gallons/1000 SCF C4+	= 0.9728	
Gallons/1000 SCF C5+	= 0.5041	
Gallons/1000 SCF C6+	= 0.2937	
Real Relative Density Gas	= 0.6932	
Unnormalized Mole Percent	= 99.547	

ACTIVE ALARMS  
 None