RECEIVED

KANSAS CORPORATION COMMISSION ONE POINT STABILIZED OPEN FLOW OR DELIVERABILITY TEST

Type Test				(+	DCC 11701	ructions on Re	verse side		_		٠		
7	en Flow			_ Test Date	n			API I	No. 15	5-2169	7 - 0	υ - <i>ο Φ</i>	
Del	liverabilt	y		Test Date	412	2013			C-P-C	-0 0 		——————————————————————————————————————	
Company	1.4	in A in	_			Sales	1-11	A			Well Num	ber -// A	
County			***************************************	رے Section		TWP	TWP R		N)	Acres Attributed		ributed	
Kinsman		40/2-5	54 54 5E				275		W		160	Ģ	
Field	الماء م	_ S y S4	J SE	Reservoir		140 100	_		ering Connec	ction			
Onciden Completion Date			Herington / Krader Plug Back Total Depth				Lumen Packer Set at						
Jan			169			none					A		
	asing Size Weight			internal E	Diameter		at 2 2 5	Perforations		16)4 OA			
	ubing Size Weight			Internal [Diameter	Set		l Perforations		To To			
		(Describe)		Type Flui	d Produc		.0(Pump Un	it or Traveling	Plunger? (Yes)	/ No		
ρυ	me!	Annulus / Tubing			7.4	water		B ()	الهردو	y Unit			
Producing	_	Annulus / Tubing خن ان ہ)	% C	arbon D	Hoxide		% Nitroge	en/ '	Gas G	ravity - G。 。)	<i>(</i> -	
Vertical D	Pepth(H)	n51 U2		Pressure Taps				V Li	/>		Run) (Pro		
	161	9		tor't tilleteste elektronocker och med andre		Flan	ال.				1.06	2	
Pressure	Buildup:	う Shut in し	4+4 2	10/3 at 9	66.1	(A) (PM)	Taken C	#	267				
Well on L		Started 6	5+4 2	013 at	`-0Đ	(AM) (PM)	Taken		20	at	(A	M) (PM)	

	<u> </u>	Circle one:	Pressure	1	OBSE	RVED SURFAC		T	ubing 1	Duration of Shut	<u>-in</u>	Hours	
Static / Orifi Dynamic Siz		Meter	Differential	Differential Flowing		ture Wellhead	Casing Wellhead Pressure		d Pressure	Duration		Liquid Produced	
Property	(inches	psig (Pm)	re in Inches H ₂ 0	1	· t	(P _w) or (I	P _t) or (P _c) psia	(P _w) or psig	(P ₁) or (P _c)	(Hours)	(Ba	rrefs)	
Shut-In							1						
Shut-In Flow	. 25					140	154.4			24			
	. 25				FLOW	140	154.4			24			
		Circle one:	Press	Grau		140	154.4		Metered Flow			Flowing	
Flow Plate Coeffiec	eient	Circle one: Meter or Prover Pressure	Extension	Grav Fac	vity tor	140 24 STREAM ATTI Flowing Temperature	154.4 RIBUTES Dev	iation ctor	Metered Flow	GOR (Cubic Fo	eet/	Fluid	
Flow	e eient	Meter or		1	vity tor	140 えせ STREAM ATTE	154.4 RIBUTES Dev	iation		GOR	eet/		
Plate Coeffiec (F _b) (F	e eient	Meter or Prover Pressure	Extension	Fac	vity tor	140 24 STREAM ATTE Flowing Temperature Factor	154.4 RIBUTES Dev	iation ctor	R	GOR (Cubic Fo	eet/	Fluid Gravity	
Plate Coeffiec (F _b) (F	e eient	Meter or Prover Pressure	Extension	Fac F	vity tor	140 24 STREAM ATTE Flowing Temperature Factor	754.4	iation ctor	R	GOR (Cubic F Barrel	eet/)	Fluid Gravity G _m	
Plate Coeffiec (F _b) (F Moto	e eient	Meter or Prover Pressure psia	Extension	Fac F	vity tor	140 24 STREAM ATTE Flowing Temperature Factor F ₁₁	754.4	iation ctor	R (Mcfd)	GOR (Cubic F. Barrel	eet/	Fluid Gravity G _m	
Plate Coeffice (F _h) (F Mcfd	eient (p)	Meter or Prover Pressure psia : (P _w) ² =	Extension P _m x h	(OPEN FL P _d =	vity tor	I/40 24 STREAM ATTE Flowing Temperature Factor Fin ELIVERABILITY % (Backpri	P _c - 14.4) + essure Curve	ATIONS 14.4 =	(Mcfd)	GOR (Cubic F. Barrel	eet/)) ² = 0.207) ² = Ope	Fluid Gravity G _m	
Flow Plate Coeffice (F_b) (F Mcfd $P_n)^2 = $ $(P_c)^2 \cdot (I_b)^2 \cdot I_b$ or	P _u) ²	Meter or Prover Pressure psia : (P _w) ² =	Extension P _m x h : Choose farmula 1 or 3 1. P _n 2 - P _n 2	(OPEN FL P _d = LOG of formula	ow) (DE	I/40 24 STREAM ATTE Flowing Temperature Factor F ₁₁ ELIVERABILITY % (Backpr. Sk	P _c - 14.4) + essure Curve corpe = "n"	ATIONS 14.4 =	(Mcfd)	GOR (Cubic F. Barrel) ² = 0.20;) ² = Oper Defive	Fluid Gravity G _m	
Plate Coeffiec (F _b) (F Mcfd	P _u) ²	Meter or Prover Pressure psia : (P _w) ² = (P _E) ² - (P _w) ²	Extension P _m x h	(OPEN FL P _d = LOG of formula 1. or 2. and divide	ow) (DE	I/40 24 STREAM ATTE Flowing Temperature Factor Fin LIVERABILIT % (Backpri Sk	Pc - 14.4) + essure Curve 2pp = "n"	ATIONS 14.4 =	(Mcfd)	GOR (Cubic Fr Barrel (P _a	eet/)) 2 = 0.207) 2 = Oper Defive Equals F	Fluid Gravity G _m 7	
Flow Plate Coeffice (F_b) (F Mcfd $P_c)^2 = \qquad \qquad$	P _u) ²	Meter or Prover Pressure psia : (P _w) ² = (P _E) ² - (P _w) ²	Extension P _m x h : Choose formula 1 or 2 1. P _n ² - P _n ² 2. P _o ² - P _o ²	(OPEN FL P _d = LOG of formula 1. or 2. and divide	ow) (DE	I/40 24 STREAM ATTE Flowing Temperature Factor Fin LIVERABILIT % (Backpri Sk	Dev Fa F P P P P P P P P P P P P P P P P P	ATIONS 14.4 =	(Mcfd)	GOR (Cubic Fr Barrel (P _a	eet/)) 2 = 0.207) 2 = Oper Defive Equals F	Fluid Gravity G _m 7 n Flow erability R x Antilog	
Flow Plate Coeffice (F_b) (F Mcfd $P_n)^2 = $ $(P_c)^2 \cdot (I_b)^2 \cdot I_b$ or	P _u) ²	Meter or Prover Pressure psia : (P _w) ² = (P _E) ² - (P _w) ²	Extension P _m x h : Choose formula 1 or 2 1. P _n ² - P _n ² 2. P _o ² - P _o ²	(OPEN FL P _d = LOG of formula 1. or 2. and divide	ow) (DE	I/40 24 STREAM ATTE Flowing Temperature Factor Fin LIVERABILIT % (Backpri Sk	Dev Fa F P P P P P P P P P P P P P P P P P	ATIONS 14.4 =	(Mcfd)	GOR (Cubic Fr Barrel (P _a	eet/)) 2 = 0.207) 2 = Oper Defive Equals F	Fluid Gravity G _m 7 n Flow erability R x Antilog	
Flow Plate Coeffice (F_b) (F McId $P_c)^2 = \frac{1}{(P_c)^2 - (1-r)^2}$	P _u) ²	Meter or Prover Pressure psia : (P _w) ² = (P _E) ² - (P _w) ²	Extension P _m x h : Choose formula 1 or 2 1. P _n ² - P _n ² 2. P _o ² - P _o ²	(OPEN FL P _d = LOG of formula 1. or 2. and divide by:	ow) (DE	I/40 24 STREAM ATTE Flowing Temperature Factor Fin LIVERABILIT % (Backpri Sk	P _c - 14.4) + essure Curve ope = "n" or or ssigned dard Slope	ATIONS 14.4 =	(Mctd)	GOR (Cubic Fr Barrel (P _a	eet/)) 2 = 0.207) 2 = Oper Defiv. Equals F	Fluid Gravity G _m 7 n Flow erability R x Antilog	
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Flow Plate Coeffice (F_b) (F Mcfd $P_c)^2 = (P_c)^2 - (I$ Open Flo	P _u) ² P _d) ² w	Meter or Prover Pressure psia : (P _w) ² = (P _E) ² - (P _w) ²	Extension P _m x h : Chaose formula 1 or 3 1. P _n ² - P _n ² 2. P _n ² - P _n ² divided by: P _n ² - P _n Mcfd @ 14	(OPEN FL Pd = LOG of formula 1. or 2. and divide by: 65 psia Company, s	OW) (DE	Flowing Temperature Factor Fin ** ** ** ** ** ** ** ** **	P _c - 14.4) + essure Curve or or ssigned dard Slope	ATIONS 14.4 =	(Mcfd)	GOR (Cubic For Barrel (Pa (Pa	eet/) 2 = 0.207 2 = Oper Defive Equals F (M	Fluid Gravity G _m 7 In Flow erability R x Antilog lcfd)	
Flow Plate Coeffice (F_b) (F Mcfd $(P_c)^2 - (I)$ Open Flo	P _u) ² P _d) ² w	Meter or Prover Pressure psia : (P _w) ² = (P _E) ²	Extension P _m x h : Chaose formula 1 or 3 1. P _n ² - P _n ² 2. P _n ² - P _n ² divided by: P _n ² - P _n Mcfd @ 14	(OPEN FL Pd = LOG of formula 1. or 2. and divide by: 65 psia Company, s	OW) (DE	Flowing Temperature Factor Fin ** ** ** ** ** ** ** ** **	P _c - 14.4) + essure Curve ope = "n" or ssigned dard Slope billity buthorized t	ATIONS 14.4 =	e above repor	GOR (Cubic F. Barrel (Pa (Pr.) Antilog Mefd @ 14.65 ps t and that he h	eet/) 2 = 0.207 2 = Oper Defive Equals F (M	Fluid Gravity G _m 7 In Flow Brability R x Antilog Idetd) dge of	
Flow Plate Coeffice (F_n) (F Mcfd $(P_n)^2 = $ $(P_c)^2 - (I$ Open Flo	P _u) ² P _d) ² w	Meter or Prover Pressure psia : (P _w) ² = (P _E) ²	Extension P _m x h : Choose farmula 1 or 2 1. P _a ² - P _a ² 2. P _a ² - P _a divided by: P _a ² - P _w Mcfd @ 14 behalf of the aid report is tru	(OPEN FL Pd = LOG of formula 1. or 2. and divide by: 65 psia Company, s	OW) (DE	Flowing Temperature Factor Fin ** ** ** ** ** ** ** ** **	P _c - 14.4) + essure Curve ope = "n" or ssigned dard Slope billity buthorized t	ATIONS 14.4 =	e above repor	GOR (Cubic F. Barrel (Pa (Pr.) Antilog Mefd @ 14.65 ps t and that he h	eet/) 2 = 0.207 2 = Oper Defive Equals F (M	Fluid Gravity G _m 7 In Flow Brability R x Antilog Idetd) dge of	

I declare under penalty of perjury under the laws of the state of Kansas that I am authorized to request exempt status under Rule K.A.R. 82-3-304 on behalf of the operator
is a coalbed methane producer is cycled on plunger lift due to water is a source of natural gas for injection into an oil reservoir undergoing ER is on vacuum at the present time; KCC approval Docket No. is not capable of producing at a daily rate in excess of 250 mcf/D I further agree to supply to the best of my ability any and all supporting documents deemed by Commission staff as necessary to corroborate this claim for exemption from testing.
Date: June 13, 2013 Signature: Stud Millond Title: AGENT

Instructions:

If a gas well meets one of the eligibility criteria set out in KCC regulation K.A.R. 82-3-304, the operator may complete the statement provided above in order to claim exempt status for the gas well.

At some point during the current calendar year, wellhead shut-in pressure shall have been measured after a minimum of 24 hours shut-in/buildup time and shall be reported on the front side of this form under **OBSERVED SURFACE DATA**. Shut-in pressure shall thereafter be reported yearly in the same manner for so long as the gas well continues to meet the eligibility criterion or until the claim of eligibility for exemption **IS** denied.

The G-2 form conveying the newest shut-in pressure reading shall be filed with the Wichita office no later than December 31 of the year for which it's intended to acquire exempt status for the subject well. The form must be signed and dated on the front side as though it was a verified report of annual test results.

KCC WICHITA

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