6206352594

## Kansas Corporation Commission One Point Stabilized Open Flow or Deliverability Test

	n Flow verabilty		,	Test Date:	-13			1 IAV	No. 15/5	Well Number  Acres Attributed				
Company	ر مر <sup>ر</sup>	oil = E	As LLC	/ -3	/-	Lease	110		, 0		Nell Number			
County		Location		Section		TWP	-/ K	RNG (E/		, , , , , , , , , , , , , , , , , , ,	Acres Attributed			
L/+/K/	<u>′</u>		14	09 Reservoir	******	<u> </u>	(	Gas Gag	ering Connect	tion	ar for the designed and shall be the first a small beautiful and a state of the sta			
completion	Per n Date	KANE	7	Morro Plug Back Tol				Packer S		STEAM	The state of the s			
11-1	07-1	1963	A	568	39			N	ove					
asing Siz	že Ž	Weight	5#	Internal Diam		Set at 52	<i>3</i> ∂	Perfor	ations	™57€	682			
ubing Siz	:e	Weight	#	Internal Diam		Set at	40	Pertor	ations	TODIA				
	pletion (D		Δ./a	Type Fluid Pr	oduction	. 1		Pump Uni	t or Traveling P	lunger? Yes	y No			
S'//roducing	Thru (An	2000 / inulus / Tubing	110 row	% Carbo	A fe		<u></u>	W/n/ % Nitroge		Gas Gra	OdO avity - G			
ANN ertical De			And the second s		on Dioxide % Nitrogen / Gas Gravity' - G <sub>g</sub> O, 00  Pressure Taps (Meter Run) (Prover) Si					Run) /Prover) Size				
5 micai De	234	<i>†</i> '	4			•				,	, , ,			
ressure E	Buildup:	Shut in 4	/. 5 <sup>2</sup> 20	13 at 9:3	30 (	AM) (PM) T	aken 4	-6-1	13 20%	3 at 9,13				
ell on Lir	ne:	Started	20	at	(	AM) (PM) T	aken	****	20	at				
				OB	SERVED	SURFACE	DATA		D	uration of Shut-	in 2.4 Hour			
Static /	Orifice Size	Circle one: Meter	Pressure Differential	- 1	II Head	Casing Wellhead Pr	- 1		ubing d Pressure	Duration Liquid Produced				
ynamic i							Coounc	AAGIILIGS	d Fiessore	Colollon	Liquio Produced			
	(inches)	Prover Pressur psig (Pm)	re in Inches H <sub>2</sub> 0	Temperature Tem t	t	(P <sub>w</sub> ) or (P <sub>1</sub> )			(P <sub>1</sub> ) or (P <sub>c</sub> )	(Hours)	(Barrels)			
roperty		1	1 3		, ,	(P <sub>w</sub> ) or (P <sub>1</sub> )	or (P <sub>c</sub> )	(P <sub>w</sub> .) or	(P <sub>1</sub> ) or (P <sub>c</sub> )		1 '			
roperty		1	1 3		, ,	(P <sub>w</sub> ) or (P <sub>1</sub> )	or (P <sub>c</sub> )	(P <sub>w</sub> .) or	(P <sub>1</sub> ) or (P <sub>c</sub> )		1 '			
Property Shut-In Flow		psig (Pm)	1 3	t	OW STRE	(P <sub>w</sub> ) or (P <sub>1</sub> ) psig  43  AM ATTRIE	or (P <sub>o</sub> )	(P <sub>w</sub> .) or	(P <sub>1</sub> ) or (P <sub>c</sub> )		(Barrels)			
roperty Shut-In	(inches)	1	1 3	t	OW STRE	(P <sub>w</sub> ) or (P <sub>1</sub> )	or (P <sub>o</sub> )	(P <sub>w</sub> ) or psig	(P <sub>1</sub> ) or (P <sub>c</sub> )		(Barrels)  Flowing Fluid Gravity			
Flow  Plate Coefficcie (F <sub>b</sub> ) (F <sub>µ</sub>	(inches)	psig (Pm)  Circle one:  Mater or rover Pressure	Press Extension	FLC Gravity Factor	OW STRE	(P <sub>w</sub> ) or (P <sub>1</sub> ) psig  AM ATTRIE Flowing mperature Factor	or (P <sub>e</sub> ) psia  BUTES  Devia Fac	(P <sub>w</sub> ) or psig	(P <sub>1</sub> ) or (P <sub>c</sub> ) psia  Metered Flow	(Hours)  GOR (Cubic Fe	(Barrels)  Flowing Fluid Gravity			
Flow  Plate Coefficcie (F <sub>b</sub> ) (F <sub>s</sub> Mcfd	(inches)	psig (Pm)  Circle one:  Mater or rover Pressure	Press Extension	FLC Gravity Factor	DW STRE	Packet Find The Packet Find Th	BUTES  Devia Fac Fn	(P <sub>w</sub> ) or psig	Metered Flow R (Mcfd)	(Hours)  GOR (Cubic Fe Barrel)	Flowing Fluid Gravity G <sub>rs</sub>			
Flow  Plate Coefficcie (F <sub>b</sub> ) (F <sub>s</sub> Mcfd	(inches)	psig (Pm)  Circle one: Maler or rover Pressure psia  (P <sub>w</sub> ) <sup>2</sup> =	Press Extension  P <sub>m</sub> x h	FLC Gravity Factor F <sub>g</sub>	DW STRE	Pactor Fit (Pc) (Pc) (Pc)	BUTES  Devia  Fac Fn  CALCULA - 14.4) +	(P <sub>w</sub> ) or psig	Metered Flow R (Mcfd)	(Hours)  GOR (Cubic Fe Barrel)	(Barrels)  Flowing Fluid Gravity G.			
Plate Coefficcie (F <sub>b</sub> ) (F <sub>s</sub> Mcfd	(inches)	psig (Pm)  Cimle one: Maler or rover Pressure psia  (P <sub>w</sub> ) <sup>2</sup> =	Press Extension  P <sub>m</sub> x h  Choose formula 1 or 2:  1. P <sub>e</sub> <sup>2</sup> - P <sub>d</sub> <sup>2</sup> 2. P <sub>e</sub> <sup>2</sup> - P <sub>d</sub> <sup>2</sup>	Gravity Factor F <sub>c</sub> (OPEN FLOW) P <sub>d</sub> =  LOG of tormula 1. or 2. and divide D and D a	DW STRE	Packpress  (P <sub>w</sub> ) or (P <sub>1</sub> ) psig  (AM ATTRIB  Flowing mperature Factor F <sub>11</sub> (P <sub>c</sub> Backpress Siope	BUTES  Devia Fac Fn  - 14.4) +  Sure Curve = "n" gned	(P <sub>w</sub> ) or psig	Metered Flow R (Mcfd)	(Hours)  GOR (Cubic Fe Barrel)	Flowing Fluid Gravity G <sub>rs</sub>			
Plate Coefficie (F <sub>b</sub> ) (F <sub>m</sub> Mcfd	(inches)	psig (Pm)  Cimle one: Maler or rover Pressure psia  (P <sub>w</sub> ) <sup>2</sup> =	Press Extension  P <sub>m</sub> x h	Gravity Factor F <sub>c</sub> (OPEN FLOW) P <sub>d</sub> =  LOG of tormula 1. or 2. and divide D and D a	OW STRE	AM ATTRIB  Flowling mperature Factor F::  RABILITY) (Pc  Backpress Siope	BUTES  Devia Fac Fn  - 14.4) +  Sure Curve = "n" gned	(P <sub>w</sub> ) or psig	Metered Flow R (Mcfd)	(Hours)  GOR (Cubic Fo Barrel)  (P <sub>a</sub> )	(Barrels)  Flowing Fluid Gravity G <sub>R</sub> 2 = 0.207 2 =  Open Flow Deliverability Equals R × Antilog			
roperty  Shut-In  Flow  Plate Coefficcie ( $F_b$ ) ( $F_a$ ) Mcfd $F_b$ ( $F_b$ )	(inches)	psig (Pm)  Cimle one: Maler or rover Pressure psia  (P <sub>w</sub> ) <sup>2</sup> =	Press Extension  P <sub>m</sub> x h  Choose formula 1 or 2:  1. P <sub>e</sub> <sup>2</sup> - P <sub>d</sub> <sup>2</sup> 2. P <sub>e</sub> <sup>2</sup> - P <sub>d</sub> <sup>2</sup>	Gravity Factor F <sub>s</sub> (OPEN FLOW) P <sub>d</sub> = LOG of tormula 1. or 2 and divide by:	OW STRE	AM ATTRIB  Flowling mperature Factor F::  RABILITY) (Pc  Backpress Siope	BUTES  Devia Fac Fn  - 14.4) +  Sure Curve = "n" gned	(P <sub>w</sub> ) or psig	Metered Flow R (Mcfd)	(Hours)  GOR (Cubic Fe Barrel)  (P <sub>a</sub> )  (P <sub>d</sub> )	(Barrels)  Flowing Fluid Gravity G <sub>R</sub> 2 = 0.207 2 =  Open Flow Deliverability Equals R × Antilog			
roperty  Shut-In  Flow  Plate  Coefficcie $(F_b)(F_a)$ Mcfd $(P_c)^2 - (P_c)^2$ $(P_c)^2 - (P_c)^2$	(inches)	psig (Pm)  Cimle one: Maler or rover Pressure psia  (P <sub>w</sub> ) <sup>2</sup> =	Press Extension  P <sub>m</sub> x h  Choose formula 1 or 2:  1. P <sub>e</sub> <sup>2</sup> - P <sub>d</sub> <sup>2</sup> 2. P <sub>e</sub> <sup>2</sup> - P <sub>d</sub> <sup>2</sup>	FLC Gravity Factor F <sub>s</sub> (OPEN FLOW) P <sub>d</sub> =  LOG of tormula 1. or 2. and divide by:	OW STRE	AM ATTRIB  Flowling mperature Factor F::  RABILITY) (Pc  Backpress Siope	or (P <sub>o</sub> ) psia  BUTES  Devia Fac Fac -14.4) + sure Curve = "n" or " orgred d Slope	(P <sub>w</sub> ) or psig	Metered Flow R (Mcfd)	(Hours)  GOR (Cubic Fe Barrel)  (P <sub>a</sub> )  (P <sub>d</sub> )	(Barrels)  Flowing Fluid Gravity G <sub>r</sub> 2 = 0.207  2 = Open Flow Deliverability Equals R x Antilog (Mctd)			
Plate Coefficies $(F_b)^2 = (P_c)^2 - (P_c)^2$	(inches)	psig (Pm)  Circle one: Meter or rover Pressure psia  (P <sub>w</sub> ) <sup>2</sup> =	Press Extension P <sub>m</sub> x h  Choose formula 1 or 2:  1. P <sub>e</sub> <sup>2</sup> - P <sub>a</sub> <sup>2</sup> 2. P <sub>e</sub> <sup>2</sup> - P <sub>a</sub> <sup>2</sup> divided by: P <sub>e</sub> <sup>2</sup> - P <sub>a</sub> <sup>2</sup>	Gravity Factor F <sub>s</sub> (OPEN FLOW) P <sub>d</sub> =  LOG of tormula 1. or 2. and divide by:	Te (DELIVE %	Packpress Siope Assignment Standard	BUTES  Devia Fac Fac - 14.4) + sure Curve = "n" or, gned d Slope	(P <sub>w</sub> ) or psig	Metered Flow R (Mcfd)	(Hours)  GOR (Cubic Fe Barrel)  (P <sub>a</sub> )  (P <sub>d</sub> )  Antilog	(Barrels)  Flowing Fluid Gravity G <sub>r</sub> 2 = 0.207  2 = Open Flow Deliverability Equals R x Antilog (Mctd)			
Plate Coefficie ( $F_b$ ) ( $F_a$ ) Mcfd $P_b = \frac{(F_b)^2}{(F_b)^2} = \frac{(P_c)^2}{(P_c)^2} = \frac{(P_c)^2}{(P_c)^2}$ Open Flow	ent Pro	psig (Pm)  Circle one: Meter or over Pressure psia  (Pw)2 =	Press Extension  P <sub>m</sub> xh   Choose formula 1 or 2:  1. P <sub>c</sub> <sup>2</sup> - P <sub>d</sub> <sup>2</sup> 2. P <sub>c</sub> <sup>2</sup> - P <sub>d</sub> <sup>2</sup> divided by: P <sub>c</sub> <sup>2</sup> - P <sub>d</sub> <sup>2</sup> Mcfd @ 14,	Gravity Factor F <sub>s</sub> (OPEN FLOW) P <sub>d</sub> =  LOG of tormula 1. or 2. and divide by:	OW STRE	Packpress Siope	or (P <sub>o</sub> ) psia  BUTES  Devia Fac Fn  - 14.4) + sure Curve = "n" gned rd Slope  ity	(P <sub>w</sub> ) or psig	Metered Flow R (Mcfd)  OG Metered Flow R (Mcfd)	(Hours)  GOR (Cubic Fe Barrel)  (P <sub>a</sub> )  (P <sub>d</sub> )  Antilog	(Barrels)  Flowing Fluid Gravity G <sub>R</sub> 2 = 0.207 2 = Open Flow Deliverability Equals R x Antilog (Mcfd)			
Plate Coefficie ( $F_b$ ) ( $F_a$ ) $P_c$ ) = $P_c$ ( $P_c$ ) $P_c$ ( $P_c$ ) $P_c$ or $P_c$	ent Pro	psig (Pm)  Circle one: Meter or over Pressure psia  (Pw)2 =	Press Extension  P <sub>m</sub> x h  :  Choose formula 1 or 2:  1. P <sub>c</sub> <sup>2</sup> - P <sub>a</sub> <sup>2</sup> 2. P <sub>c</sub> <sup>2</sup> - P <sub>a</sub> <sup>2</sup> divided by: P <sub>c</sub> <sup>2</sup> - P <sub>a</sub> <sup>2</sup> Mcfd @ 14.  In behalf of the aid report is true	FLO Gravity Factor F <sub>g</sub> (OPEN FLOW) P <sub>d</sub> =  LOG of tormula 1. or 2. and divide by:	OW STRE	Packpress Siope	or (P <sub>o</sub> ) psia  BUTES  Devia Fac Fn  - 14.4) + sure Curve = "n" gned rd Slope  ity	(P <sub>w</sub> ) or psig	Metered Flow R (Mcfd)  OG Metered Flow R (Mcfd)	(Hours)  GOR (Cubic Fe Barrel)  (P <sub>a</sub> )  (P <sub>d</sub> )  Antilog	(Barrels)  Flowing Fluid Gravity G <sub>R</sub> 2 = 0.207 2 = Open Flow Deliverability Equals R x Antilog (Mcfd)			

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I declare under penalty	of perjury under the laws of the state of Kansas that I am authorized to request	
exempt status under Rule K	A.R. 82-3-304 on behalf of the operator	
	ssure information and statements contained on this application form are true and	
correct to the best of my kn	owledge and belief based upon available production summaries and lease records	
of equipment installation an	d/or upon type of completion or upon use being made of the gas well herein named.	
I hereby request a one-	year exemption from open flow testing for the Tutyle 1-9	
gas well on the grounds the		
(Check one)		
is a coal	bed methane producer	
is cycled	d on plunger lift due to water	
	rce of natural gas for injection into an oil reservoir undergoing ER	
	cuum at the present time; KCC approval Docket No.	
4 Is not ca	pable of producing at a daily rate in excess of 250 mcf/D	
	y to the best of my ability any and all supporting documents deemed by Commission	on .
starr as necessary to corro	borate this claim for exemption from testing.	
2 12 1	of	وعدون
Date: 3 - 17 - //		
	M. W.	
	Signature:	
	Title: MANA 9en	

Instructions:

If a gas well meets one of the eligibility criteria set out in KCC regulation K.A.R. 82-3-304, the operator may complete the statement provided above in order to claim exempt status for the gas well.

At some point during the current calendar year, wellhead shut-in pressure shall have been measured after a minimum of 24 hours shut-in/buildup time and shall be reported on the front side of this form under **OBSERVED SURFACE DATA**. Shut-in pressure shall thereafter be reported yearly in the same manner for so long as the gas well continues to meet the eligibility criterion or until the claim of eligibility for exemption **IS** denied.

The G-2 form conveying the newest shut-in pressure reading shall be filed with the Wichita office no later than December 31 of the year for which it's intended to acquire exempt status for the subject well. The form must be signed and dated on the front side as though it was a verified report of annual test results.

KCC WICHITA

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