KANSAS CORPORATION COMMISSION ONE POINT STABILIZED OPEN FLOW OR DELIVERABILITY TEST

Type Test	:					(See Inst	ructi	ons on Re	verse Sid	e)						
✓ Open Flow				Test Date: API No. 15													
Deliverabilty				2/20 to 2/21/14					007-23,133-00-00								
Company Pollok E		, LL	С						Lease Benson	1				3-9	Well Nu	ımber	
County Location Barber SWNWSW				Section 9			TWP 35S	,			Acres Attributed						
Field , Aetna Gas Area					Reservoir Miss/Cherokee				Gas Gathering Conne Atlas			า					
Completion Date 7/03/07					Plug Bac 5072	k Total [Depth	n Packer Set at none			Set at						
Casing Size Weight 4.5				······································	Internal Diameter			Set :	at 9		Perforations 4882		т _о 4993				
Tubing Size Weight 2.375					Internal Diameter			Set at 4860			Perforations		То				
Type Con single	npletio	n (De	escribe)			Type Flui Oil/SW	Type Fluid Production				Pump Unit or Traveling PI Yes - pump unit			Plunger? Yes / No			
	Thru	(Anı	nulus / Tubii	na)			arbon D	ioxic	de	<u> </u>	% Nitrogen			Gas Gravity - G			
annulus		(,		.51		.098					1.851			.646			
Vertical Depth(H)				Pressure Taps flange								(Meter Run) (Prover) Size 2"					
Pressure	Buildu	p:	Shut in	17	2	0_14_at_1		<u>_</u> _		Taken_2	/20	20	14	at 10:15	am	(AM) (PM)	
Well on L	ine:	•	Started 2/2	20		0 <u>14</u> at <u>1</u>						20				(AM) (PM)	
							OBSE	RVE	SURFAC	E DATA			Dura	ation of Shut-	_{in} _72	Hours	
Static / Orifi			_ Meter		Pressure Differential in	Flowing Temperature			Casing Wellhead Pressure (P _w) or (P ₁) or (P _c)		Wellh	Tubing Wellhead Pressure (P,) or (P,) or (P,)		Duration (Hours)		Liquid Produced (Barrels)	
Property (inche		es) Prover Pres psig (Pm		1		t t		psig		psia	psig			(110015)		(50.7010)	
Shut-In	yt-In								601.3	615.7			72				
Flow	Flow .375		22.5		11.2	31	31		171.1	185.5			24				
					······································		FLOW	STRI	EAM ATTR	RIBUTES							
Plate Coeffiecient (F _b) (F _p) Mcfd		Circle one: Meter or Prover Pressure psìa			Press Extension ✓ P _m x h	Gravity Factor F _o		Flowing Temperature Factor F ₁₁		Fa	viation actor F _{pv}			w GOR (Cubic Fee Barrel)		Flowing Fluid Gravity G _m	
.6860		36	36.9		20.33	1.244		1.029			18					<u> </u>	
						(OPEN FL	OW) (DE		······································	CALCIII	ATIONS	1				<u>i</u>	
$(c_c)^2 = _{0}^{2}$	79.086	<u> </u>	(P _w)²	3	34.410 :	P _d =		%		P _c - 14.4) +		:		(P _a):	2 = 0.2 2 =	07 	
$(P_c)^2 - (P_a)^2$ or $(P_c)^2 - (P_d)^2$		(P _c) ² - (P _w) ²		:	nose formula 1 or 2: 1. $P_c^2 - P_a^2$ 2. $P_c^2 - P_d^2$ the d by: $P_c^2 - P_a^2$	LOG of formula 1. or 2. and divide by: Pc²-Pw²		2	Backpressure Ci Slope = "n" or Assigned Standard Slop		n x LOG		Antilog		Open Flow Deliverability Equals R x Antilog (Mcfd)		
378.879		344.676		1.099		.0409			.850		.03	.0347		1.08		19	
									Assigr	ned							
pen Flov	_v 19				Mcfd @ 14.0	65 psia	<u></u>		Deliverat	oility			Mcfd	@ 14.65 psi	а		
		•	•						•		// _	he above repo	ort an	d that he ha			
e facts st	ated t	herei	in, and that s	aid	report is true	and correc	t. Execu	ited 1	this the $\frac{2}{}$	6th	May of F	ebruary	ŀ			20	
			Witness	(if any	у)			_	-		lly	William For	Compan	у	(CC	WICH	
			For Com	missic	on			-	-	2	evm,	Che	cked by		MAR	WICH 0 6 2014	
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Meter Analysis

January, 2014

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	Mol %	Liquid Content		
Carbon Dioxide	0.098	0.0167	Pressure Base	14.730
Nitrogen	1.851	0.2036	Temperature Base	60.00
Methane	88.470	14.9945		
Ethane	5.492	1.4683	•	
Propane	2.301	0.6338	Relative Density	0.6463
Iso-Butane	0.263	0.0861	Dry Heating Value	1124.09
N-Butane	0.703	0.2215	As Del Heating Value	1121.37
Iso-Pentane	0.163	0.0595	Sat Heating Value	1104.53
N-Pentane	0.227	0.0823		
Hexane	0.432	0.1884	•	
Heptane			C2+ Liquid Content	2.7399
Octane			C5+ Liquid Content	0.3302
Nonane			C6+ Liquid Content	0.1884
Decane			26# Gasoline	0.5229
Oxygen			H2S ppm	1.0
Hydrogen				
Helium				
Argon				
Water Vapor				
Hydrogen Sulfide				

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